

Computational compliance criteria in water hammer modelling

Kamil Urbanowicz^{1,*}

¹West Pomeranian University of Technology, Szczecin, Faculty of Mechanical Engineering and Mechatronics,
 Al. Piastów 17, 70-310 Szczecin, Poland

Abstract. Among many numerical methods (finite: difference, element, volume etc.) used to solve the system of partial differential equations describing unsteady pipe flow, the method of characteristics (MOC) is most appreciated. With its help, it is possible to examine the effect of numerical discretisation carried over the pipe length. It was noticed, based on the tests performed in this study, that convergence of the calculation results occurred on a rectangular grid with the division of each pipe of the analysed system into at least 10 elements. Therefore, it is advisable to introduce computational compliance criteria (CCC), which will be responsible for optimal discretisation of the examined system. The results of this study, based on the assumption of various values of the Courant-Friedrichs-Levy (CFL) number, indicate also that the CFL number should be equal to one for optimum computational results. Application of the CCC criterion to own written and commercial computer programmes based on the method of characteristics will guarantee fast simulations and the necessary computational coherence.

1 Introduction

When water flow is started or stopped faster than the system can respond acoustically, a pressure surge commonly referred to as a water hammer event will occur. The same principle is also applicable when the flowing medium is another fluid (oil, steam etc., in the case of steam, the pressure surge is known as a steam hammer event). In the mentioned transient state, water hammer waves – also called pressure waves – are transmitted through the system at the speed of sound of the water-pipe combination. In typical steel pipes, the pressure wave speed is greater than 1200 m/s. This pressure waves can cause major problems, from noise and vibration to pipe collapse and total system failure.

This is the reason why the protection of water systems or nuclear power plants cooling systems against water hammer is so important. Designers of such a pressurised systems normally use expensive additional equipment to protect them against water hammer damage: hydro-pneumatic or surge tanks, special valves, air chambers, rupture disks [1, 2]. But the simplest, effective and nearly cost free protection is to control the valve-closing time and the pump speed. For optimal control procedures at the stage of designing such systems, a numerical simulation analysis is needed [3, 4].

It is assumed that the flow of this type is being described by the hyperbolic system of partial differential equations (sequentially by the continuity equation and the motion equation) [1-6]:

$$\frac{\partial p}{\partial t} + \rho c^2 \frac{\partial v}{\partial x} = 0, \quad (1)$$

$$\frac{\partial p}{\partial x} + \rho \frac{\partial v}{\partial t} + \rho g \sin \gamma + \frac{2}{R} \tau_w = 0, \quad (2)$$

where:

p – pressure [Pa], t – time [s], ρ – density [kg/m³], c - pressure wave speed [m/s], v - flow velocity [m/s], x - axis coordinate [m], g - acceleration due to gravity [m/s²], γ - pipe tilt [°], R - inner radius [m], τ_w - wall shear stress [Pa].

Direct solutions of this equations are not known at present, therefore the method of characteristics (MOC) is used most often which, when initial and boundary conditions are properly selected, allows numerical solution of these equations. The MOC technique is now widely known but yet is not entirely clarified, which will be shown by the tests performed in this study.

Like any numerical method, it must meet the necessary requirements that will ensure the stability and adequate accuracy (compliance) of the results being obtained. The literature [1, 2, 5, 6] presents the stability criterion in the form of:

$$CFL = \frac{c \Delta t}{\Delta x} \leq 1, \quad (3)$$

where:

Δt – time step [s], Δx – single reach length (horizontal distance between neighbouring grid nodes) [m].

The exemplary simulations performed in this study indicate that this criterion should be rather written in the form of equality. As for the compliance criterion, it is difficult to find in the current literature on this subject any condition which would have to be satisfied to maintain necessary simulation accuracy. As shown by the results of the comparative tests performed and

Corresponding author: kamil.urbanowicz@zut.edu.pl

discussed in this paper, an additional criterion should be associated with compaction on the length of pipe of the numerical grid of the characteristics.

The objective of this study is therefore to answer the question on what division should be considered appropriate that the simulation results being observed are characterised by an acceptable compliance with those obtained by experimental tests.

2 Computational compliance criteria

2.1 Difference between stability and compliance of results

Stability is one of the most important properties of dynamic systems. In the case of unsteady flow, especially during the water hammer event examined in this study, the pipe flow which after brining it from the steady state tends over time to another steady state, being characterised by another flow velocity, is considered the stable one. The concept of stability of the unsteady flow caused by rapid valve closure can also be defined by setting relevant requirements for the courses of pressure changes (as well as for the courses of average velocity value) in the examined cross-sections. Nevertheless, the pressure changes that take place in the systems where during water hammer events no cavitation caverns are formed should be always accompanied with time by a gradual decrease in maximum pressures at successive amplitudes. However, in the pressure runs with cavitation, maximum pressures at the second or the third amplitude (that occur after the first column separation) can not be higher than twice the value being determined using the Joukowski equation. The said oversized increase in pressure is being explained by the fact of superposition of a greater number of pressure waves [7], because any closure of the cavitation area is a source of the next wave. Superposition of waves results in the fact that the stability of exponential maximum pressure envelope, typical for the pressure runs without cavitation, is not observed in the cavitation courses. Also in the case of pipe flows with cavitation, there is a typical pressure drop at the time of flow deceleration after the occurrence of maximum amplitude.

Within the problem being analysed in this study, the stability of numerical solutions of the differential equations that describe the water hammer event should be mentioned as well. And here, the stability of solution should be understood as continuous dependence of the solution on set initial conditions.

In this connection, the stability criterion is not responsible for the accuracy of modelling but only for its correctness in the mathematical sense. Following the analysis of the method of characteristics (which is used to numerically solve the partial equations that describe the water hammer), as well as the results being obtained themselves, it is reasonable therefore to introduce another criterion, the objective of which would be to guarantee compliance between simulated results and those being observed experimentally.

2.2 Purpose and scope of the study

Unfortunately, the studies that used the method of characteristics to model the unsteady pipe flows have not indicated at what minimum division the results being obtained will be characterised by an acceptable error. Simpson and Bergant [8] modelled the pipe flows with cavitation assuming different computational elements (Table 1). They observed, when applying the division into 32 elements and more, that there are significant deviations and a significant variation in the results being obtained. This fact is explained by them that the greater the number of divisions into grid reach lengths, the more cavitation areas is modelled and, at the same time, the greater is the likelihood of a superposition of waves. They suggested that the number of reaches (grid points) over the pipe length (N) is to be chosen so that the ratio of the maximum cavitation volume being modelled to the volume of fluid contained in a single numerical element is to reach the value below 10%. Interestingly, they did not notice any modelling problems when applying division into 4 or 8 elements. In 2001, in another study – this time on the pipe flows without cavitation-related column separation, Bergant et al. [9] applied the division only into N = 8, 16 and 32 elements and showed that different number N on the diamond (staggered) grid, using the friction model according to Brunone, does not affect the quality of simulated pressure runs (Fig. 1).

Table 1. Discretisation and cavitation and friction models applied in other studies.

Year [Paper]	Author's initials	Grid	Friction model	Number of reaches N	Cavitation model
1994 [8]	S.A.R. – B.A.	R; S	Q-S	4,8,16,32, 64,128,256	SM; DVCM, DGCM
1996 [10]	B.M. – A.A.*	R	BM	3,5,8,10,12 14,16,20	DVCM
2001 [9]	B.A. et al.	S	CT (Z); BM	8,16,32	No cavitation
2006 [11]	A.A. – L.M.	S	Q-S; CT (Z; V-B); BM	12,24,36	No cavitation
2007 [13]	H-T.L. et al.	FD L-W	Q-S	10,20,40	DBCM
2009 [14]	H-T.L.-H-T.E.	FD L-W	Q-S	6,12,24,40	DBCM
2012 [12]	A.A. – L.M.	S	Q-S CT (Z; V-B)	17,33,65	DACM
2014 [15]	K.U. et al.	S	CT (Z; V-B; V)	54,108,216 432, 864	DGCM
2015 [16]	B.A. – K.U.	S	CT (Z; V-B; V)	32, 64, 96	DGCM

Legend:

Initials: S.A.R.-Simpson Angus R.; B.A.-Bergant Anton; A.A.-Adamkowski Adam; L.M.-Lewandowski Mariusz; H-T.L.-Hadj-Taieb Lamljed; H-T.E.-Hadj-Taieb Ezzeddine; K.U.-Karadzic Uros; B.M.-Bughezem Mohamed; A.A.*-Anderson Alexander

Grid: R-rectangular; S-staggered (diamond); FD L-W – Finite difference Lax- Wendroff scheme

Friction models: Q-S – quasi-steady; BM – Brunone’s model; CT – Convolution type; Z – Zielke model; V-B – Vardy-Brown model; V – Vitkovský model

Cavity models: SM – Streeter model; DVCM – Discrete vapour cavitation model; DBCM – Discrete bubbly cavitation model; DGCM – Discrete gas cavitation model; DACM – Discrete Adamkowski cavitation model

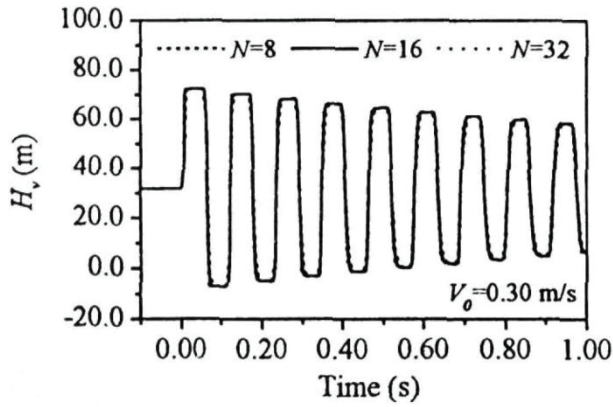


Fig. 1. Bergant et al.'s results for different N [9].

Bughazem and Anderson [10] pointed to a significant effect of N on simulation results based on a series of tests performed on the rectangular grid of the characteristics (they used the friction model according to Brunone). Adamkowski and Lewandowski, when examining the effect of friction on simulation results of the pressure runs without cavitation [11], observed no effect of the grid density on the simulation compliance and the stability of numerical computations when applying the division into $N = 12, 24$ and 36 . In their next comparative study on the pipe flows with cavitation [12], the same authors showed that the division of N, however, affects the time of modelling the transition from the course with cavitation into the course without it (Fig. 2).

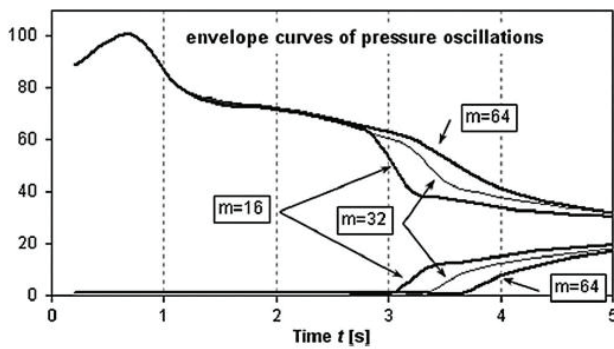


Fig. 2. Envelope of the analysed pressure curve obtained for different N [12].

The significant effect of N on simulation results (Fig. 3, Fig. 4) has been also observed by Hadj-Taieb et al. [13, 14], but these authors did not use the method of characteristics and solved the basic equations with the finite-difference method (Lax-Wendroff method). However, while analysing the results obtained by Karadžić et al. [15], it is clear that also for the relatively dense division $N = 54, 108$ and 216 significant difference between the simulated results can be seen (Fig. 5).

In other studies, their authors often forget to specify which numerical discretisation was used to perform comparative tests [17-20] or they only show the applied

number of divisions without commenting its effect on the results being obtained [21-23].

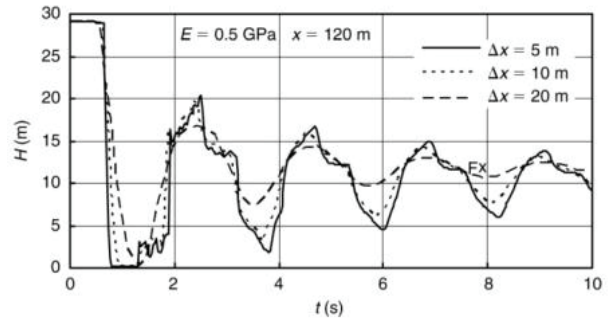


Fig. 3. Hadj-Taieb's et al. 2007 results [13].

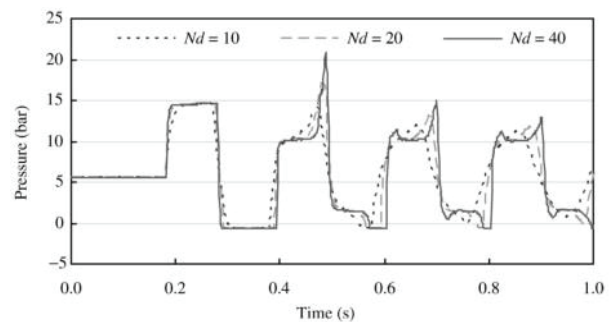


Fig. 4. Hadj-Taieb's 2009 results [14].

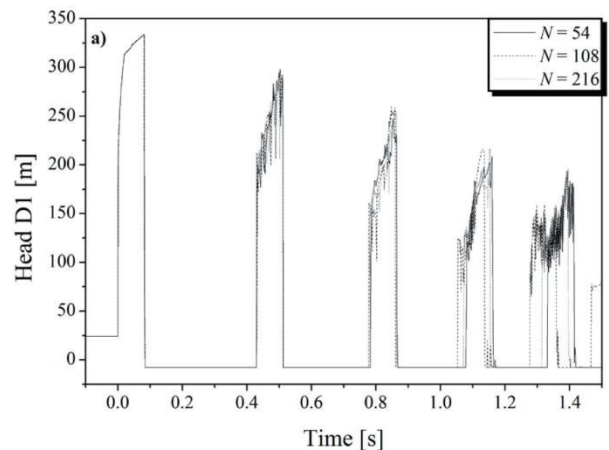


Fig. 5. Variation of results for large N [15].

Summing up, the following three important conclusions can be drawn from the studies being analysed:

- no significant effect of N on simulation results is being noticed in the pressure runs without cavitation [9, 11];
- the effect of N seems to be much larger in the pressure runs with cavitation, although this does not refer to the modelling of the first amplitudes being characterised by maximum pressures but rather to the time of transition of the courses with cavitation-related column separation into the courses without cavitation [8, 12, 15];

– the method of characteristics is less sensitive to the change of N factor than other methods (for example, the finite-difference method – the studies by Hadj-Tajeb [13, 14]).

On the basis of the literature being reviewed above, the objective and scope of the study could be defined.

The purpose of tests performed and described in this study was to determine the optimum value (number) of the numerical division of hydraulic pipe (of the sample length L) into computational elements (marked in this study as N). This division should be as small as possible so that the computer calculations that use the method of characteristics are to be made as fast as possible.

Owing to the fact that the rectangular grid of the characteristics is commonly used and the effect of N on them was analysed according to Table 1 only in two studies, the tests being described in the next section will be carried out just on it.

Some authors, including Vítkovský [24-26], have suggested that the rectangular grid is the result of the overlapping of two diamond grids (staggered-diamond grid) and, according to them, this affects simulation results. Own experiments presented in this study as well as in previous ones [17, 19, 22] do not show, however, any problem associated with the rectangular grid. Commonly, a sharp toothed increase in pressure is being observed on the peak of the first pressure amplitude on the rectangular grid. This drawback can be minimised, however, by showing on the graph illustrating the variation of pressure in a given pipe cross-section being analysed every second simulated result. Then, a smoothed simulation waveform will be obtained, very similar to the results being obtained on the diamond grid. The scope of the study will refer to the comparative analysis of a number of courses being modelled (with and without cavitation; laminar, transient and turbulent: $1100 < Re_i < 40350$) with the experimental ones being obtained in a typical hydraulic system.

2.3 Effect of number of reaches on simulation results

In the tests presented below, the hydraulic pipe being examined was divided into N computational elements, starting from N = 2, every 1, to N = 64. Carrying out computer simulation in such a wide range guaranteed an accurate picture of the variation of two basic quantitative parameters: Et and Ep, being determined for each simulated pressure run. Parameters Ep (maximum pressure compliance) and Et (time compliance) characterise compatibility of the pressure runs being modelled [19]. They are calculated using the experimental and numerical results (Fig. 6) from the following formulas:

$$Ep = \frac{\sum_{i=1}^k \left| \frac{p_{is} - p_{ie}}{p_{ie}} \right| \cdot 100\%}{k}, \quad (4)$$

$$Et = \frac{\sum_{i=1}^{k-1} \left| \frac{t_{is} - t_{ie}}{t_{ie}} \right| \cdot 100\%}{k-1}, \quad (5)$$

where:

k - number of analysed pressure amplitudes; p_{is} and p_{ie} - maximum pressure on the i-th analysed amplitude from the simulated and experimental graph, respectively; t_{is} and t_{ie} - time of occurrence of the maximum pressure on the i-th analysed amplitude from the simulated and experimental graph, respectively.

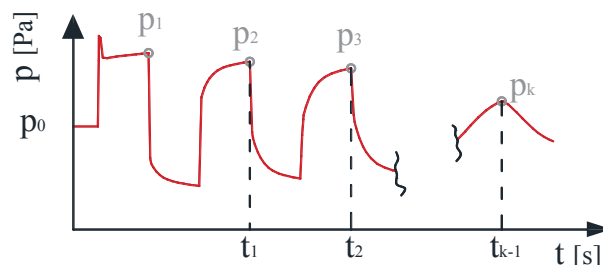


Fig. 6. Analysed pressure and times values in the quantitative analysis.

In his study, when determining parameter Et, the time compliance on the first amplitudes was omitted because the chosen experimental results used for comparisons were characterised by a noticeable effect of the vibrations of the valve being closed on the initial phase of pressure curve (fluid structure interaction (FSI) effect).

Experimental tests necessary for comparative analysis have been performed by Adamkowski and Lewandowski at the Institute of Fluid-Flow Machinery of the Polish Academy of Sciences in Gdańsk. In their paper of 2006 [11], these authors showed courses, in which cavitation-related column separation did not occur. From that study, nine courses were selected for the comparisons being made in this study (Table 2). However, in the study of 2012 [12], the same authors showed different results obtained on a slightly modified test bench, in which cavitation-related column separation occurred. In the comparative tests presented below, six courses obtained then were used (Table 3). The details necessary for numerical modelling are compiled in the presented tables (Table 2 and 3). The values of pressure wave propagation speed c, which were used in computations, collected in the Tables 2 and 3 were not calculated from theoretical equations but determined by the analysis of experimental pressure runs.

Table 2. Experimental details for cases without cavitation.

NO CAVITATION (L = 98.11 m; D = 0.016 m; $\rho = 997.65 \text{ kg/m}^3$; $\nu = 9.493 \cdot 10^{-7} \text{ m}^2/\text{s}$; k = 16)		
v_0 [m/s]	c [m/s]	p_T [Pa]
0.066	1305	$1.2647 \cdot 10^6$
0.162	1304	$1.2642 \cdot 10^6$
0.340	1304	$1.265 \cdot 10^6$
0.467	1308	$1.253 \cdot 10^6$
0.559	1306	$1.264 \cdot 10^6$
0.631	1307	$1.2641 \cdot 10^6$
0.705	1305	$1.263 \cdot 10^6$
0.806	1306	$1.263 \cdot 10^6$
0.940	1304	$1.264 \cdot 10^6$

Owing to the fact that this study examined the effect of N on the pressure runs with cavitation, it was necessary to implement additional conditions for determination of the volumes of emerging cavitation areas in the computer programme being used to solve the basic equations describing the unsteady flow of that type. As a model of cavitation-related damage of the flow continuity, the model according to Adamkowski-Lewandowski was used, which has been described in detail in the paper of 2009 [27].

Table 3. Experimental details for cases with cavitation.

WITH CAVITATION ($L = 98.56$ m; $D = 0.016$ m; $\rho = 1000$ kg/m ³ ; $\nu = 1.09 \cdot 10^{-6}$ m ² /s)			
v_0 [m/s]	c [m/s]	p_T [Pa]	k
0.47	1260	$2.44 \cdot 10^5$	13
0.82	1250	$2.42 \cdot 10^5$	12
1.03	1230	$2.43 \cdot 10^5$	11
1.7	1240	$4.23 \cdot 10^5$	12
1.9	1240	$4.23 \cdot 10^5$	11
2.74	1260	$7.03 \cdot 10^5$	13

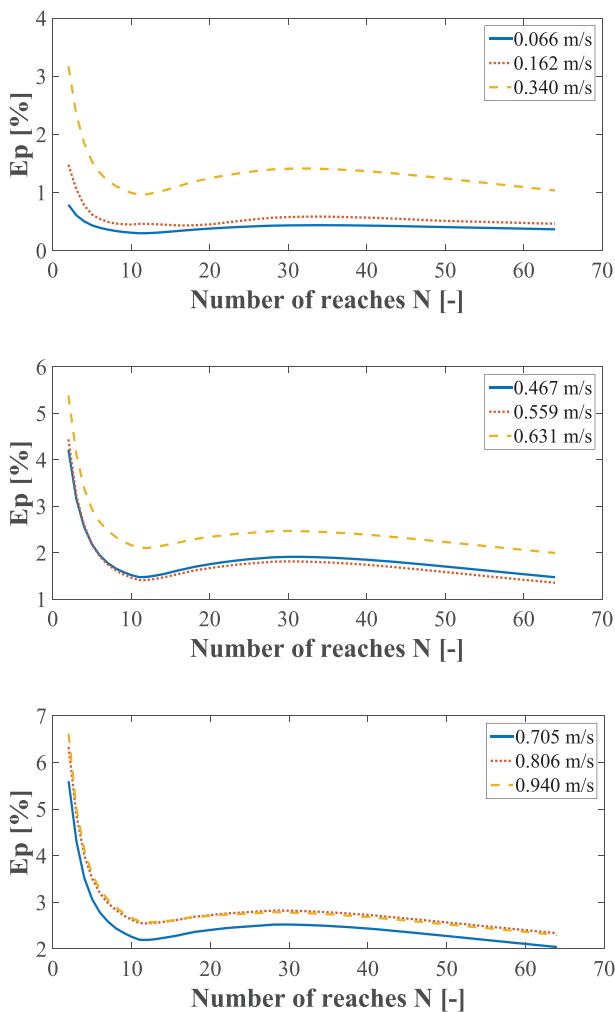


Fig. 7. Results for E_p (cases without cavitation).

The Table 2 shows that the average value of pressure near the reservoir p_T was $1.263 \cdot 10^6$ [Pa] and that the differences observed in the speed of pressure wave propagation (1304-1308 m/s) were slight (from the average value of 1305.44 m/s, the error was only $\pm 0.2\%$). For the tests with cavitation-related column separation (Table 3), it can be concluded that the differences being observed experimentally in the speed of pressure wave propagation were significant in relation to those without cavitation (from the average value of 1246.667 m/s, the error was $\pm 1.36\%$). In the tests being performed, dispersion of the values of pressure wave propagation speed c was as much as 30 m/s, suggesting that there are bubbles of air in the flowing fluid in the chosen pressure runs, in which the propagation speed was the lowest because this is mainly them that decrease the speed of pressure wave propagation.

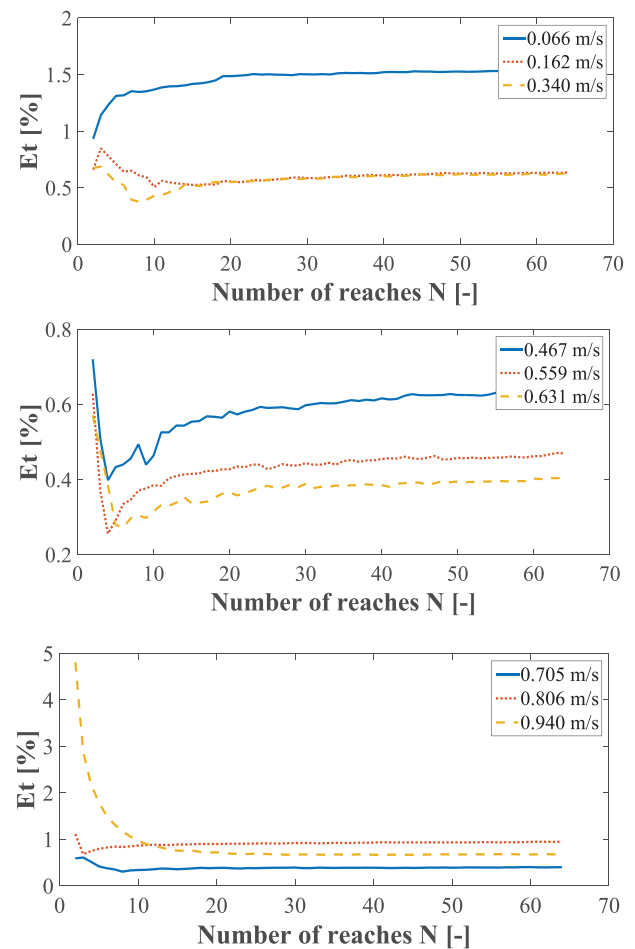


Fig. 8. Results for E_t (cases without cavitation).

The detailed results of the variation of parameters E_p and E_t in the function of changes in the grid density N of the characteristics are shown by two presented graphs (Fig. 7 and Fig. 8). In the comparative tests, the time and the amplitude compliances of these pressure amplitudes which occurred in first five seconds from the valve closure were analysed. In the courses without cavitation, the number of the analysed amplitudes was the same for all carried out runs, i.e. $k=16$, whereas in the courses

with cavitation their number varied depending on the boundary and initial conditions (for k values see Table 3).

On the other hand, the next two graphs show the variation of the same parameters but for the courses in which column separation occurred, i.e. there were cavitation areas appearing (Fig. 9 and Fig. 10).

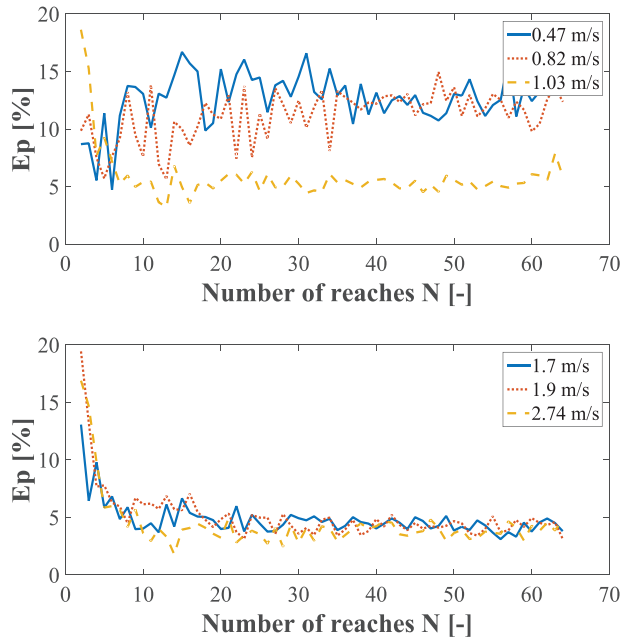


Fig. 9. Results for E_p (cases with cavitation).

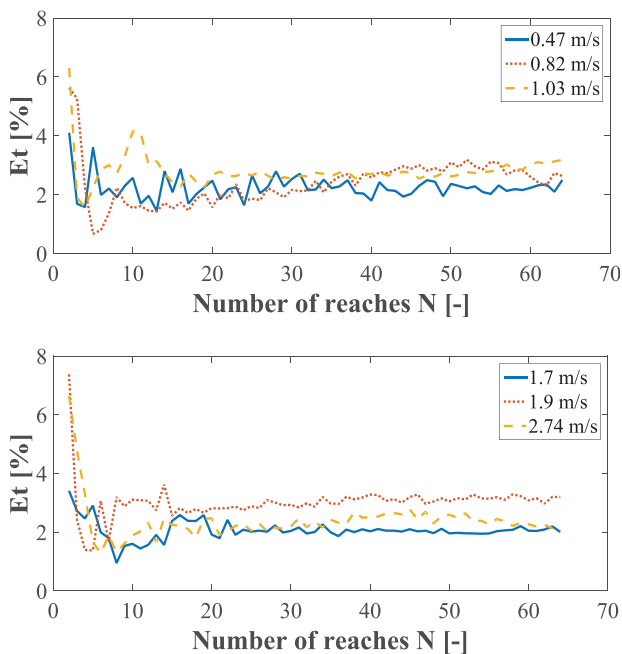


Fig. 10. Results for E_t (cases with cavitation).

From the results of quantitative tests shown in a graphical form (Fig. 7 to Fig. 10), the following conclusions can be drawn:

- in the pressure runs without cavitation, the acceptable compliance of simulations with the experimental results was obtained for the division into $N = 10$ (Fig. 7 and Fig. 8). Analysis of the variation of parameter E_p (Fig. 7) shows that this error will be smaller for $N > 60$. On the other hand, analysis of the variation of parameter E_t (Fig. 8) showed that with the increasing N in five runs ($v_0 = 0.162; 0.34; 0.467; 0.559; 0.631$) there was a slight but steady increase in the error. However, it can be considered that the E_t results being obtained for $N = 10$ were characterised by acceptable values;
- analysis of the results obtained for courses with cavitation (Fig. 9 and Fig. 10) showed that in these runs the results can be accepted if division of the pipe is assumed at 10 elements ($N = 10$) although smaller dispersion of the results in these analysed runs is visible for $N > 20$;
- pressure runs with cavitation in the transitional range ($v_0 = 0.47; 0.82$) are characterised by unacceptable modelling errors E_p within the ranges of 8% to 16% and a high sensitivity to changes in parameter N (Fig. 9). This may suggest the need of further work on improving the applied cavitation model for the range of transitional pipe flows.

3 Effect of the Courant-Friedrichs-Lewy (CFL) number

The Courant-Friedrichs-Lewy (CFL) number expresses the ratio of the distance traveled by a disturbance in one time step to the length of a computational distance step. As pointed in many textbooks, the CFL number in the method of characteristics should be less than or equal to unity [1, 2, 5, 6] so as to ensure that the solution remains within the computational domain. However, the exemplary numerical simulations performed in this study, consisting in the application of the CFL number from the following range $0.5 < CFL \leq 1$ (the following values were adopted for the tests: $CFL = 1, 0.95, 0.9, 0.85, 0.8, 0.7, 0.6$ and 0.5) for the same simple system, showed that the application of lower value of the CFL number results only in deterioration of the modelling errors – higher values of parameters E_p and E_t . The input values for the simulation being performed were assumed as follows: $c = 1245$ [m/s], $\rho = 1000$ [kg/m³], $\nu = 1.09 \cdot 10^{-6}$ [m²/s], $N = 32$ [-], $L = 98.56$ [m], $R = 0.08$ [m], $v_0 = 1.9$ [m/s], and $p_T = 4.23 \cdot 10^5$ [Pa]. The selected simulation results are presented in Figure 11.

It is clear from this graph that with the decreasing CFL number the next simulated pressure amplitudes appear faster. The transformed CFL condition L (Eq. 3), while assuming appropriate discretisation of the grid over the pipe length Δx and the pressure wave propagation speed c , has the following form:

$$\Delta t \leq \frac{\Delta x}{c} \Rightarrow \Delta t \leq \frac{L}{N \cdot c}, \text{ because: } \Delta x = L/N, \quad (6)$$

where:

L – pipe length [m], N – number of reaches (grid nodes) [-].

It is clear from this formula that each reduction of time step (equivalent to adoption of lower CFL number) results in numerical calculations such as adoption of another length of the hydraulic pipe being examined. In order to avoid errors of the above type, the CFL condition in the case of using the rectangular grids of the characteristics with fixed computational mesh must be associated with the adoption CFL number equal to unity:

$$\frac{\Delta t \cdot c}{\Delta x} = 1. \quad (7)$$

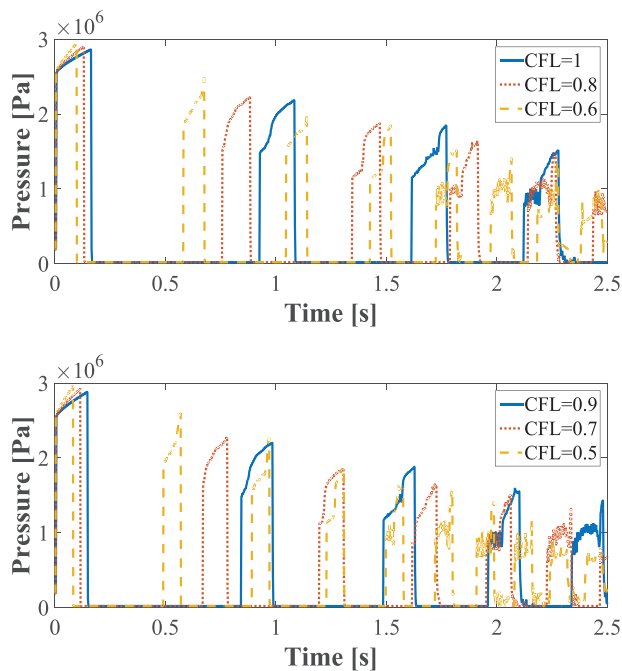


Fig. 11. CFL number effect.

4 Conclusions

A number of simulations performed in this study helped to determine a numerical criterion of the compliance of simulated results. The computation compliance criterion CCC enforces at the beginning of numerical calculations the necessary division of pipe into computational elements. According to the test results being observed in the method of characteristics for rectangular grids, the following condition must be satisfied:

$$N \geq 10.$$

An additional condition, which was demonstrated in section 3, is to maintain the stability criterion in the form of the Courant-Friedrichs-Lewy number equal to unity (CFL = 1).

In order to confirm the condition defined above in a wider range, further tests for pipes with other lengths, as well as other internal diameters, are necessary.

In addition, the performed tests clearly show that the unsteady pressure runs without cavitation are simulated with a greater accuracy; this may suggest that there is a need for modification of the cavitation model according to Adamkowski-Lewandowski so that the error for the Reynolds number, especially from the range of

transitional flow (multiple transition from the laminar flow in the turbulent one during the pressure pulsation dumping is a phenomenon that accompanies the water hammer event) is also below the acceptable range of 5%.

References

1. E.B. Wylie, V.L. Streeter, L. Suo, *Fluid Transients in Systems* (Prentice Hall, 1993)
2. M.H. Chaudhry, *Applied Hydraulic Transients* (Springer, 3rd ed., 2014)
3. Z. Zarzycki, S. Kudźma, K. Urbanowicz, J. Theor. App. Mech-Pol. **49**, 135 (2011)
4. K. Urbanowicz, Z. Zarzycki, J. Theor. App. Mech-Pol. **50**, 487 (2012)
5. S. Mambretti, *Water Hammer Simulations* (WIT Press, 2014)
6. R.H. Pletcher, J.C. Tannehill, D. Anderson, *Computational Fluid Mechanics and Heat Transfer* (Taylor and Francis, 3rd ed., 2013)
7. A.R. Simpson, E.B. Wylie, J. Hydraul. Eng. **117**, 1310 (1991)
8. A.R. Simpson, A. Bergant, J. Hydraul. Eng. **120**, 361 (1994)
9. A. Bergant, A.R. Simpson, J.P. Vitkovský, J. Hydraul. Res. **39**, 249 (2001)
10. M.B. Bughazem, A. Anderson, *Proc. 7th Int. Conf. Pressure Surges, BHR Group, Harrogate, England*, 537 (1996)
11. A. Adamkowski, M. Lewandowski, J. Fluids Eng. **128**, 1351 (2006)
12. A. Adamkowski, M. Lewandowski, J. Hydraul. Eng. **138**, 935 (2012)
13. L. Hadj-Taieb, E. Hadj-Taieb, C. Thirriot, Int. J. Simul. Model. **27**, 347 (2007)
14. L. Hadj-Taieb, E. Hadj-Taieb, Int. J. Simul. Model. **29**, 263 (2009)
15. U. Karadžić, V. Bulatović, A. Bergant, Stroj. Vestn. J. Mech. E. **60**, 742 (2014)
16. A. Bergant, U. Karadžić, *Proc. 12th Int. Conf. Pressure Surges, BHR Group, Dublin, Ireland*, 639 (2015)
17. K. Urbanowicz, Z. Zarzycki, S. Kudźma, J. Theor. App. Mech-Pol. **50**, 889 (2012)
18. A. Keramat, A.S. Tijsseling, Q. Hou, A. Ahmadi, J. Fluid Struct. **28**, 434 (2012)
19. K. Urbanowicz, Z. Zarzycki, J. Theor. App. Mech-Pol. **53**, 295 (2015)
20. S. Henclik, J. Theor. App. Mech-Pol. **53**, 543 (2015)
21. K. Weinerowska-Bords, J. Fluids Eng. **137**, 054501 (2015)
22. K. Urbanowicz, M. Firkowski, Z. Zarzycki, J. Phys.: Conf. Ser. **760**, 012037 (2016)

23. H. Wang, L. Zhou, D. Liu, B. Karney, P. Wang, L. Xia, J. Ma, C. Xu, *J. Hydraul. Eng.* **142**, 04016036 (2016)
24. J.P. Vítkovský, M. Lambert, A.R. Simpson, A. Bergant, *Proc. 8th Int. Conf. Pressure Surges, BHR Group, The Hague, Netherlands*, 471 (2000)
25. J.P. Vítkovský, M. Stephens, A. Bergant, M. Lambert, A.R. Simpson, *Proc. 9th Int. Conf. Pressure Surges, BHR Group, Chester, UK*, 405 (2004)
26. J.P. Vítkovský, M. Stephens, A. Bergant, A.R. Simson, M. Lambert, *J. Hydraul. Eng.* **132**, 709 (2006)
27. A. Adamkowski, M. Lewandowski, *J. Fluids Eng.* **131**, 071302 (2009)