# Design Optimization and Demand Side Management of a Solar-Assisted Industrial Heating Using Agent-Based Modelling (ABM): Methodology and Case Study

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**Abstract.** Heavy dependence on traditional fuels as well as connection to a significantly unreliable and inefficient grid (with about 20% energy loss) characterizes the Ethiopian industry. On the contrary, the country has many solar-suited industries for process heat augmentation in the low-to-medium temperature ranges. Thus, if properly designed and operated, solar thermal could give an opportunity for an efficient and cleaner alternative in these industries. This paper presents agent-based modeling (ABM) for an integrated optimization and demand side management (DSM) framework for solar-assisted industrial heating under varying load and weather condition. To demonstrate the validity and practicality of the proposed solution, a case study was conducted on Ethiopian textile industry. A payback period of 5.3 years and solar fraction of 66.7% was identified for an optimized system. Further with the implementation of DSM to guide the production policy of the industry, a 7.5% and 8.4% improvement in payback and solar fraction was achieved.

### **1** Introduction

Global estimate for industrial energy use indicates that more than 66.7% of the total energy consumption is for process heat, out of which 50% is for low-to-medium temperature range [1]. According to the same study, about two-fifths of primary energy use in industries comes from natural gas or petroleum indicating a solar replication potential that is estimated to be 15EJ which would cover about 10% of industrial energy requirement by 2030.

Identified promising industrial sectors for solar integration are: food, beverages, paper, textile, brick and blocks, chemical, plastic and flour by products [1-2]. Similar to other developing countries, these industrial sectors dominate the Ethiopian industry [3].

According to existing forecasts, the electricity consumption in Ethiopian industrial sector is expected to grow by approximately 9 folds of the 2015 consumption by 2030[4]. However, these industries are connected to the significantly unreliable national grid [5]. Consequently, the supply disruptions during the production process result in huge loss to the industries. The said unreliability of the electricity supply in the country has compelled many industries to set up their own emergency backup systems and often the diesel generator is their preferred choice. The employment of alternative local energy resources (for example, the use of solar thermal technologies to deliver industrial heat requirement, etcetera) as well as demand side management (DSM) could solve this problem.

If properly designed and operated, renewable energy resources could give an opportunity for an efficient and cleaner alternative together with the aspired reliability as is in the power industry.

The work of this paper is an attempt to address three related issues that still need a research attention. First of all, the number and fragmented nature of solar promising industrial processes have resulted in a need for a sector specific solution [1-2, 6-12]. Then more importantly, gaining the benefits of these specific solutions requires a holistic optimization framework; an approach that considers the daily performance based on weather prediction, hot water consumption variation and temperature dynamics of the thermal system. Finally, investigating the performance reliability of these optimized solutions in the presence of uncertainties in energy generation and consumption is necessary. However, scarcely few studies have answered these research questions mainly due to the inability of existing tools to handle such task [13-15]. On the other hand, agentbased models, as derivatives of complexity science, has been shown to be well suited for a natural description of systems where there is a dynamic interaction to result in complex collective patterns [15]. The primary aim of this paper is to demonstrate the capability of agent-based hybrid models for optimization and DSM analysis of an industrial scale solar thermal system. These agents have continuous thermal and consumption models that are embedded and run in parallel. Data for modelling are from measurements taken at the chosen industry and some are manufacturer's datasheet. An optimization from experiment with the total annualized cost (operating and investment) was carried out to find the optimal collector area and storage volume. These optimal parameters are then exported back to the simulation environment to investigate the possibility for improved energy use by implementing DSM to guide the industry's production policy.

### 2 Case study

The investigated dyeing textile process case study is found at Bahir Dar textile factory, in northern Ethiopia (11°36'N 37°24'E). The textile factory manufactures 100% cotton products, including yarns and fabrics. Electricity, diesel and furnace oil (FO) are the major energy source to the plant with annual consumptionn of 27.54million kWh, 166kL and 615kL respectively [17]. The textile plant has installed FO fired steam boiler for dying section. This boiler operates only during production of dying section and consumes an average of 250 litters FO per day running with efficiency below 70%. Increase price and poor reliability of FO are the two main problems that challenge the dyeing section of the textile factory. On the other hand, the textile site receives an average direct and diffused solar radiation of 6.8kWh/m<sup>2</sup> and 1.7kWh/m<sup>2</sup> [18].Thus it is easy to see that a solar thermal system would have a higher replication potential for replacing the existing inefficient FO based boiler for the dyeing section of the factory. The primary aim of this study is for optimal design of a solar thermal system for the dyeing textile process and demand side management (DSM) for further energy efficiency improvement opportunity. The dyeing machine parameter is depicted in Table 1.

### 3 Methodology

The structure of the implemented methodology is depicted in Fig -1. The implementation is modelled in a computational framework based on Anylogic 8.1 and embedded optimizer OptQuest. The proposed work is divided into four basic procedures: i) Agent definition and communication, ii) Optimization, iii) demand side management (DSM), and iv) performance evaluation.



Fig. 1. The implemented framework.

#### 3. 1 Agent definition and communication

This task involves identifying which parts of the solarassisted industrial heating is important and creating these objects in the model as agents known as generation, storage, and consumption agents. The agent definition task creates these agents having a continuous thermal and/or demand models with embedded discrete events that run in parallel.

#### 3.1.1 Generation agent

The generation agent used is Evacuated Tube Collector (ETC). ETC is the most efficient and convenient solar collector for low-to-medium temperature ranges [19]. The quasi-dynamic equation for ETC can be determined from [20, 21].

$$\begin{split} Q(t) &= \eta_0 k_{\theta b}(\theta) I_b + \eta_0 k_{\theta d}(\theta) I_d - a_1 (T_{coll} - T_{amb}) - \\ a_2 (T_{coll} - T_{amb})^2 &- c_{eff} \frac{dT_{coll}}{dt} \end{split}$$
(1)

The collector parameters for the modeling of the generation agent are taken from [16].

Table 1. Dyeing textile machine parameters		
Parameters	Values	
Mean daily production, m <sup>2</sup>	9,406	
Hot water cons, L/Kg	8 -12	
Process temp, °C	40 -60	
Minimum fabric weight, g/m <sup>2</sup>	265	
Maximum fabric width, m	2.45	
Average washing machine speed, m/min	60	
Machine efficiency, %	75	

#### 3.1.2 Storage agent

As reported in [11] a stratified storage tank helps to store solar heat efficiently and ensure lowest possible inlet temperature to collector. Thus, the storage agent is modeled as N equally segmented storage tank layers with thermal dynamics,  $T_n$ , given as

$$m_n c_p \frac{dT_n}{dt} = \dot{Q}_{conv,n} + \dot{Q}_{cond,n} - \dot{Q}_{loss,n}$$
(2)

Where the convective, conductive, and loss stated in Eqn. (2) can be determined from temperature dynamics of neighboring segments ( $T_{n-1}$  and  $T_{n+1}$ ) given by Eqns.(3-5).

$$\dot{Q}_{conv,n} = \dot{m}_c c_p (T_{n+1} - T_n) - \dot{m}_w c_p (T_n - T_{n-1}) \quad (3)$$

$$\dot{Q}_{cond,n} = \frac{T_{str,c}n}{d} (T_{n-1} + T_{n+1} - 2T_n)$$
(4)

$$\dot{Q}_{loss,n} = UA_{str,s}(T_n - T_{amb}) \tag{5}$$

This storage agent is composed of N segment chain where each segment's temperature state is derived from its own as well as the neighboring segments temperature dynamics. The first and last segment has the generation and consumption agent as the connecting Chain.

#### 3.1.3 Consumption agent

The consumption agent has three states namely idle, not available, and processing. The idle states represents the waiting mode while the dyeing machine waits inputs from other textile processes proceeding it (desizing, bleaching, washing and drying). The not available state results when the dyeing machine is periodically maintained, occasionally breakdown or randomly stopped when the factory supply power is off. The final state i.e. processing state executes continuous dyeing in accordance input parameters listed in Table 1. While in this state, the thermal energy demand of the dyeing machine is updated in the agent. Once the input fabric is entirely processed, an event will be triggered to transit the dyeing machine to the idle state. The consumption agent estimates the dyeing machines availability and hence determines its thermal energy demand.

Once the agents are defined, the remaining step is to establish the agents' communication. This communication aims at smooth interaction among agents to make them able to react to external events such as thermal energy demand from consumption agent to storage agent. In order to accomplish this task, the agent communications generates and share these patterns as well as register their status

#### 3.2 Optimization

The optimization tool used is OptQuest optimizer which is embedded into Anylogic 8.1. This optimizer is metaheuristics and is able to generalize under uncertainty during the optimization task.

An optimization experiment with total annual cost (annualized capital cost plus operating cost) of the thermal system is formulated. Both operating and investment cost for heat exchanger network, collector area, storage volume, including the control system and piping costs are considered in the objective function of the optimization experiment. The cost of investment for heat exchanger, Cex, is calculated using [21] as

$$C_{ex} = e + f * \left(\frac{A_{tot}}{N_{min}}\right)^g * N_{min} \tag{6}$$

Whereas the cost for the collector and storage,  $C_i$ , can be approximated using the power low equation that relate

the base size cost,  $C_b$ , and cost exponent factor, s, given by Eqn. (7) [11].

$$C_i = C_b \left(\frac{S_i}{S_b}\right)^n \tag{7}$$

The annualized capital cost,  $C_A$ , of a new installation over a fixed period, m, at a fixed rate of interest, i, is given by

$$C_{A} = C_{i} \frac{i(1+i)^{m}}{(1+i)^{m} - 1}$$
(8)

On the other hand, the operating cost, COP, is composed of the energy cost of auxiliary heat demand from boiler,  $C_{aux}$ , and maintenance cost,  $C_{main}$ , of the thermal system determined as

$$C_{OP} = C_{aux} + C_{main} \tag{9}$$

$$C_{energy} = C_{FO} \frac{Q_{FO}}{\eta_b} \tag{10}$$

The cost of maintenance is assumed to be 1.5% of the fixed capital investment.

#### 3.3 Demand Side Management (DSM)

The aim of DSM implementation is to reformulate the production policy of the dyeing textile process in order to use the available solar thermal energy efficiently. This is done by implementing a flexible production strategy that is in line with the seasonal and daily variation of the available solar energy. Thus, the DSM effort attempts to dynamically shift in time and/or vary the daily production rate. The allowable production rate is indirectly determined from the consumption agent that is described in section A.3. This DSM effort will result in efficient utilization of the generated solar energy thereby decreasing the associated loss.

#### 3.4 Performance Evaluation

The optimal solar thermal configuration for the considered case study is determined at the optimization step as discussed in section 3.2. Afterwards the economic analysis, solar performance and carbon dioxide saving potential of the identified optimal configuration are calculated. The payback period, the total analyzed cost and the investment cost are indicators of the economic performance whereas solar gain and solar fraction points to the extent of solar energy utilization. On the other hand, the annual carbon dioxide emission reduction indicates the GHG mitigation potential of the proposed solar thermal system. The final step involves investigating the improvement in the aforementioned performance parameters when a DSM strategy is implemented.

#### 4 Results and discussion

The first part of this section discusses the optimization result that gives the most economically feasible solution. Secondly, the demand side energy management is elaborated that leads to energy efficiency improvement potential in the considered dyeing textile process.

The optimization approach as discussed in section B was used to determine the most economical values for collector area and solar tank volume. The procedure was applied for ETC coupled to stratified storage tank with demand generated from the consumption agent.

The data shown in Table 2 gives an output of this optimization procedure.

 Table 2. Summary of results.

	Ref.	With
	system	DSM
Optimized values		
Collector area (m <sup>2</sup> )	323	323
Solar tank volume (m <sup>3</sup> )	18.1	18.1
Solar system performance		
Solar heat gain(MWh/p)	142.1	167.6
Solar fraction (%)	66.7	75
Economic analysis		
Investment cost (€)	176838	176838
Annualized total cost (€/p)	52095	52095
Payback period (p)	5.3	4.9
Saving		
Fossil fuel (MWh/p)	203.4	141.5
Cost(€/p)	9899	9830
Co <sub>2</sub> (t/p)	52.0	47.0

Before investigating DSM in the dyeing textile process, a flexible production policy needed to be formulated. This policy results from the knowledge of the dyeing machine's daily and monthly availability as estimated by the consumption agent. This consumption agent considers all stochastic events such as shortage of input fabric for the dyeing machine and represents them in probability distributions. The agent also takes deterministic events such periodic maintenance and represents them as occurrences with a given rate. The monthly dyeing machine availability is portrayed in Fig. 2.



Fig. 2. Dyeing machine availability.

After estimating the machine's availability, the DSM procedure is implemented as follow: First, the consumption agent generates thermal demand based on the maximum daily dyeing machine's availability and tries to satisfy its demand from the storage agent (coupled to the

generation agent). The excess of demand over supply is backlogged. On the succeeding days, the DSM procedure reviews the demand and supply inventory levels and decides on the daily production rate of the dyeing machine. This procedure goes on trying to match solar energy supply with production to arrive at a flexible production policy that results in maximum use of the generated solar energy. Thus, implementing the DSM strategy to guide the dyeing textile process, a maximum of 8.4% solar fraction with about 65.4MWh solar gain improvement could be achieved. Fig. 3 shows the monthly possible solar gain of the DSM implementation.



Fig. 3. DSM implementation for solar gain improvement.

## **5** Conclusions

The overall aim of this work was to arrive at an integrated optimization and demand side management approach, for decision support, in solar-assisted industrial heating. Demonstrated by a case study, it was found out that a payback period of 5.3 years and solar fraction of 66.7% was identified for an optimized system. With the implementation of DSM, to guide the production policy of the industry, a 7.5% and 8.4% improvement in payback and solar fraction was achieved.

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## Nomenclature

A Area (m<sup>2</sup>)

 $a_1, a_2$  Thermal loss coefficients (W/(m<sup>2</sup> K), W/(m<sup>2</sup> K<sup>2</sup>))

e, f, g Fixed, scaling and, non-linear cost parameter

C Cost ( $\in$ )

- $C_{FO}$  Specific cost of natural gas ( $\mathcal{C}$ /J)
- $C_p$  Specific heat capacity (J/(kg K))
- $C_{eff}$  Effective thermal capacity KJ/(m<sup>2</sup>K)

*I* Solar irradiance (W/m<sup>2</sup>)

- *i* Rate of interest
- k Thermal conductivity (W/(m K))

- $k_{\theta b, k\theta d}$  Direct and diffused incidence angle modifier
- *d* Sstorage segment distance (m)
- *n* Cost exponent factor
- *N* Number of heat exchanger
- $\dot{m}$  Mass flow (kg/s)
- *m* Number of years
- Q Heat (J)
- $\hat{Q}$  Heat flow (W)
- *S* Cost scaling factor
- *T* Temperature (°C)
- U Heat transfer coefficient (W/(m<sup>2</sup> K))

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