

Simulation of thermodynamic systems with a thermoelectric converter based on the Peltier element for energy efficient management

Alexander Lukyanov^{1,*}, *Danila Donskoy*¹, *Vitaly Bykador*¹ and *Mikhail Chuveyko*¹, and *Elena Kasyanenko*¹

¹Don State Technical University, Rostov-on-Don, Russia

Abstract. This article deals with the problem of dynamic control of thermodynamic systems based on the Peltier element. The existing methods of relay and PWM control of this object are ineffective and subject the thermoelectric converter to gradual degradation due to transients during switching off and on of the element [1]. The model of a continuous regulator we have created will allow changing the characteristics of the system to determine its behavior for various environmental input parameters. And the use of systems based on continuous control will increase the energy efficiency of the thermoelectric converter and will increase its service life.

1 Introduction

The thermoelectric converter - Peltier element is currently causing great interest when creating small systems (with a small volume) with automatic control of microclimate parameters. The main difficulties in creating such systems are complex physical principles of the thermoelectric converter itself. Therefore, when creating climate control systems, they are usually limited to stationary states of the element and the task of the control itself is lost, since Peltier works only at a certain power. Thus, the efficiency of the use of the Peltier element is very small, they consume more power, throughout the entire time of work. Our model allows us to determine the behavior of the system with various external factors and, if necessary, select the coefficients of the continuous controller for the dynamic control of the Peltier element. This minimizes energy costs and increases the energy efficiency of using this element in conjunction with continuous management.

2 Mathematical description of the heat balance of a system consisting of a storage device in a closed space and external heat exchange with the environment

The amount of heat inside the accumulator (accumulated in the structures inside the closed space):

* Corresponding author: alexlukjanov1998@gmail.com; dand22@bk.ru

$$Q_{in} = m_v c_v \theta_{in}, \quad dQ_{in} = m_v c_v \cdot d\theta_{in} \quad (1)$$

Where m_v and c_v - the mass and heat capacity of the tree, respectively.
 Heat flow providing heat exchange with the external environment through the installation walls

$$q_1 = S \frac{A}{d} (\theta_{air} - \theta_{out}) \quad (2)$$

Where S, A and d - area, thermal conductivity and thickness of expanded polystyrene (penoplex), respectively.

The mathematical model of the Peltier element can be obtained by the least squares method from the experimentally obtained data of the temperature difference depending on the current strength. This characteristic is presented in Figure 1.

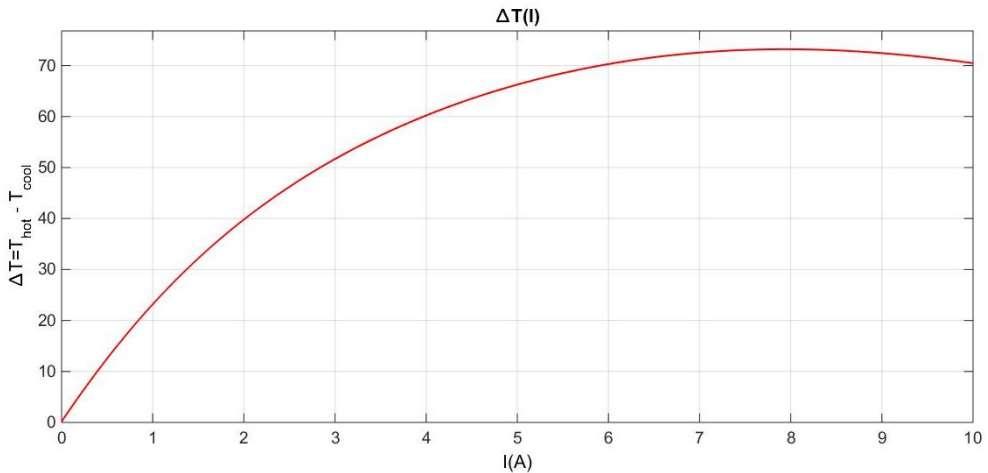


Fig. 1. Graph of the temperature difference from the current strength on the Peltier element.

Consider the heat flow pumped / pumped out by the Peltier element. In this case, we have two streams, one of which is direct, due to the transfer of heat from the hot radiator to the cold one, the other is the reverse, due to the Peltier effect. The characteristic presented in Figure 1 is described quite accurately by a third-order equation:

$$q_2 = S_p \frac{A_p}{d_p} (\theta_{hot} - \theta_{cool}) - a_1 i - a_2 i^2 - a_3 i^3 \quad (3)$$

Where $S_p \frac{A_p}{d_p} \approx 1$ - Peltier element characteristic, coefficients a_1, a_2, a_3 - coefficients obtained by the least squares method from the experimentally obtained characteristics of the Peltier element. ($a_1 = 24.67, a_2 = -2.764, a_3 = 0.1017$)

The heat exchange between the external radiator and the external environment is described by the flow:

$$q_5 = S_{Rhot} (\alpha_0 + \alpha_1 v_{Rhot}) (\theta_{hot} - \theta_{out}) \quad (4)$$

The heat exchange between the internal radiator and the internal environment is described by the flow:

$$q_4 = S_{Rcool}(\alpha_0 + \alpha_1 v_{Rcool})(\theta_{in} - \theta_{cool}) \tag{5}$$

$(\alpha_0 + \alpha_1 v_{Rcool})$ – heat transfer coefficient in moving air.
 The amount of heat stored in radiators is described, respectively, by the expressions:

$$Q_{hot} = m_{hot}c_{hot}\theta_{hot}, \quad dQ_{hot} = m_{hot}c_{hot}d\theta_{hot} \tag{6}$$

$$Q_{cool} = m_{cool}c_{cool}\theta_{cool}, \quad dQ_{cool} = m_{cool}c_{cool}d\theta_{cool} \tag{7}$$

The amount of heat stored in the air inside the unit is:

$$Q_{air} = V_{air}\rho_{air}c_{air}\theta_{air}, \quad dQ_{air} = V_{air}\rho_{air}c_{air}d\theta_{air} \tag{8}$$

The change in the density and heat capacity of air is neglected.

The heat exchange between the air and the storage structures will be described by the flow:

$$q_3 = S(\alpha_0 + \alpha_1 v_{in})(\theta_{in} - \theta_{air}), \quad v_{in} \cong v_{Rcool}/10 \tag{9}$$

LED power:

$$q_6 = P_{LCD}I_{LCD} \tag{10}$$

System Flow Chart (Fig. 2):

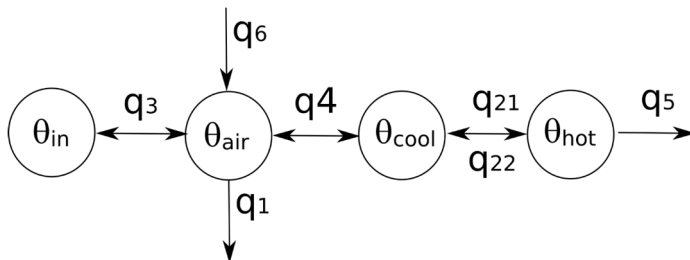


Fig. 2. The structure of the thermodynamic system model.

For convenience, the constants and variables of the model are shown in Table 1.

Table 1. Model parameters [2]

№	Name	Designation		Value (range)	Dimension
		In the article	In the model		
1	Physical constants				
1.1	heat transfer coefficient in resting air	α_0	a_0	5.6	W/(m ² K)
1.2	heat transfer coefficient to moving air	α_1	a_1	4	W/(m ² K)
1.3	air heat capacity	c_{air}	c_air	1000	J/(kg *K)
1.4	air density	ρ_{air}	ro_air	1.28	kg/m ³
1.5	thermal conductivity of plates and Peltier element material	A_p	A_p	1.875	W/(m * K)
1.6	thermal conductivity of penoplex	A	A	0.032	W/(m * K)

1.7	aluminum heat capacity	C_{AL}	c_al	920	J/K
1.8	tree heat capacity	C_{wood}	c_wood	2300	J/K
2	Technical characteristics of the experimental sample				
2.1	installation air volume	V_{air}	V_air	0.1	m ³
2.2	outer shell area	S	S	1.272	m ²
2.3	wooden structure area	S_{wood}	S_wood	0.1	m ²
2.4	area of internal radiator cooling	S_{cool}	S_cool	0.4	m ²
2.5	external radiator cooling area	S_{hot}	S_hot	0.4	m ²
2.6	Peltier element area	S_p	S_p	0.0016	m ²
2.7	Peltier thickness	d_p	d_p	0.003	m ²
2.8	penoplex thickness	d	d	0.03	m
2.9	mass of wood	m_{wood}	m_wood	0.2	kg
2.10	the mass of the internal cooling radiator	m_{cool}	m_cool	0.300	kg
2.11	mass of external radiator cooling	m_{hot}	m_hot	0.300	kg
2.12	maximum power of LEDs	P_{LED}	P_led	50	W
3	Impacts				
3.1	air velocity inside the unit	V_{in}	v	0.01	m/s
3.2	internal radiator air flow rate	V_{cool}	v_cool	3	m/s
3.3	external radiator air flow rate	V_{hot}	v_hot	3	m/s
3.4	Peltier current	i_p	i_p	≤4	A
4.5	the intensity of the use of LEDs (from 0 to 1)	I_{LED}	I_led	0 – 0.05	-
3.6	ambient temperature	θ_{out}	Teta_out	20	°C
3.7	initial temperature conditions	θ_0	Teta_0	Teta_out	°C
4	Model state variables				
4.1	temperature of structures	θ_{wood}			
4.2	air temperature inside	θ_{air}			
4.3	cold radiator temperature	θ_{cool}			
4.4	hot radiator temperature	θ_{hot}			
4.5	Peltier current	i_p			
4.6	integral regulator	X_{PI}			

Let's make the equations of the system, to facilitate their form, simplify the expression of constants:

$$CM = \frac{1}{m_{wood}c_{wood}} \quad (11)$$

$$Sv = S_{wood}(a_0 + a_1v_{in}) \quad (12)$$

$$Sc = S_{cool}(a_0 + a_1v_{cool}) \quad (13)$$

$$Sh = S_{hot}(a_0 + a_1 v_{hot}) \tag{14}$$

$$Pq = S \frac{A}{d} \tag{15}$$

$$Pp = S_p \frac{A_p}{d_p} \tag{16}$$

$$Aq = \frac{1}{V_{air} \rho_{air} c_{air}} \tag{17}$$

$$Mc = \frac{1}{m_{cool} c_{Al}} \tag{18}$$

$$Mh = \frac{1}{m_{hot} c_{Al}} \tag{19}$$

$$Led = P_{LED} I_{LED} \tag{20}$$

In general, the system of equations describing the processes of this system is:

$$\left\{ \begin{array}{l} \frac{d\theta_{wood}}{dt} = -CM * Sv(\theta_{wood} - \theta_{air}) \\ \frac{d\theta_{air}}{dt} = Aq(Sv(\theta_{wood} - \theta_{air}) - Pq(\theta_{air} - \theta_{out}) - Sc(\theta_{air} - \theta_{cool}) + Led) \\ \frac{d\theta_{cool}}{dt} = Mc(Sc(\theta_{air} - \theta_{cool}) - Pp(\theta_{cool} - \theta_{hot}) - a_1 i - a_2 i^2 - a_3 i^3) \\ \frac{d\theta_{hot}}{dt} = Mh(Pp(\theta_{cool} - \theta_{hot}) + a_1 i + a_2 i^2 + a_3 i^3 - Sh(\theta_{hot} - \theta_{out})) \\ \frac{di_p}{dt} = k_p(\theta_{air} - \theta_z) + X_{PI} \\ \frac{dX_{PI}}{dt} = k_i(\theta_{air} - \theta_z) \end{array} \right. \tag{21}$$

The last two equations describe the PI controller to control the Peltier element.

2 The result of mathematical modeling

The system was studied at an external temperature of 20 degrees with a fluctuation of ± 5 over a long period of time (10^5 seconds). The Peltier element was required to bring the temperature of the internal environment of the system to 25 °C set by us. As a result of modeling the system were obtained graphs of energy consumption. Comparative graphs of energy consumption with continuous and relay control can be seen in Figure 3. Savings amounted to 5.6%

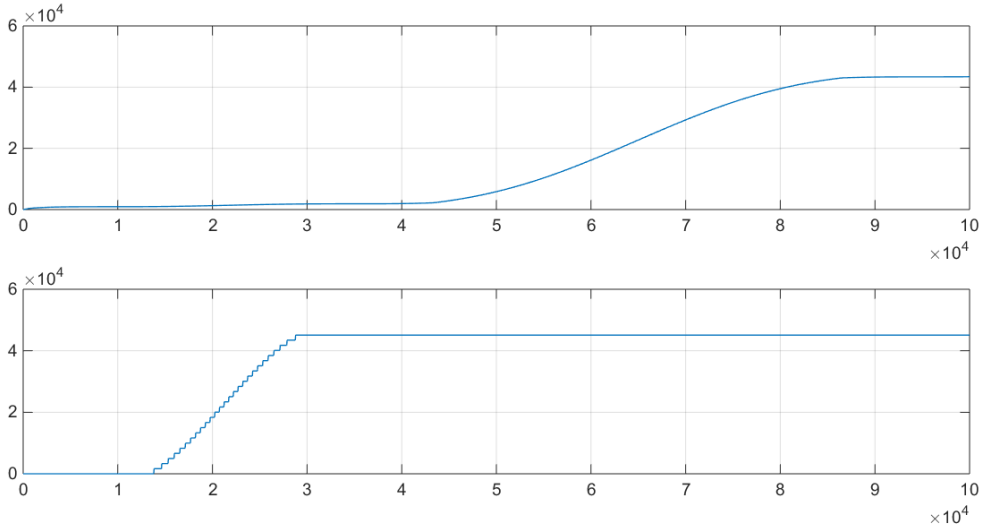


Fig. 3. Energy efficiency of various control methods: 1) continuous method (PI - regulation), 2) Relay method.

5 Conclusion

Thus, we have developed a universal model for analyzing the processes occurring when using semiconductor thermoelectric converters. The power consumed in the continuous control of the thermoelectric converter is 5.6% lower than in the case of relay control, since systems with this element have a large inertia. The model presented by us will allow creating scalable complexes of microclimate maintenance systems that are quite economical and useful both in everyday life and in creating automated greenhouse systems, for example, for preparing and germinating seedlings. The use of continuous control allows you to significantly save on the power consumption of the Peltier element and increase its service life.

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