

# Investigating the zinc ion adsorption capacity of a chitosan/ $\beta$ -cyclodextrin complex in wastewater

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**Abstract.** To decrease the amount of  $Zn^{2+}$  in industrial waste water, in this study,  $\beta$ -cyclodextrin ( $\beta$ -CD) was first modified and then used to obtain a  $\beta$ -cyclodextrin polymer ( $\beta$ -CDP). The effects of reaction temperature and reaction time of  $\beta$ -CD with citric acid (CA), polyethylene glycol 400 (PEG-400), and disodium hydrogen phosphate ( $NaH_2PO_4$ ) on the amount of  $\beta$ -CDP produced were investigated. The results showed that at a reaction temperature of 145 °C and a reaction time of 4.5 h, 6.58 g of  $\beta$ -CDP was produced. Then, chitosan (CTS) was crosslinked with  $\beta$ -CDP using glutaraldehyde to prepare a chitosan/ $\beta$ -cyclodextrin (CTS/ $\beta$ -CDP) complex. The mass ratio of CTS to  $\beta$ -CDP, reaction temperature, reaction time, and amount of added glutaraldehyde were used as the main variables to examine the  $Zn^{2+}$  adsorption rate and adsorption capacity of the composites prepared in this study. The optimum experimental conditions were as follows: a mass ratio of 3:10, a reaction temperature of 80 °C, a reaction time of 90 min, and 2 mL of glutaraldehyde. Under these optimal conditions, the adsorption amount and adsorption rates of  $Zn^{2+}$  using CTS/ $\beta$ -CDP complex were respectively 97.70  $mg \cdot g^{-1}$  and 78.92%.

## 1 Introduction

The mechanical manufacturing, papermaking, chemical, and battery manufacturing industries produce large amounts of heavy metal ions such as  $Zn^{2+}$ , which is a highly toxic, non-degradable, and persistent pollutant. It causes serious environmental damage and can also enter humans through the food chain when it pollutes rivers and lakes, which seriously endangers human health [1-2]. Currently, common methods for removing  $Zn^{2+}$  from waste water include electrolysis, ion exchange, chemical precipitation, adsorption, and electrodialysis [3-4]. However, these methods are complicated and produce large amounts of solid waste, and are plagued by high costs and energy consumption. CTS and  $\beta$ -CD are natural products with high adsorption abilities that do not cause secondary water pollution. Thus, in recent years, they have been used to treat domestic and industrial wastewater containing heavy metal ions, dyes, phenols, organic matter, and similar pollutants. CTS is abundant in nature, and is the only natural alkaline polysaccharide [5-7]. Its molecular chain contains many functional groups, including amino and hydroxyl groups, and it can electrostatically adsorb or complex with heavy metal ions. When combined with heavy metals in water [8], it has an excellent adsorption ability and a high mechanical strength, but it does not have a selective adsorption. The structure of  $\beta$ -CD contains a hydrophobic cavity which, along with its peripheral hydroxyl groups, can remove heavy metal ions from aqueous systems [9-12]. Modified  $\beta$ -CDP maintains the cavity and recognition ability of

$\beta$ -CD, and also has good mechanical strength and stability [13], but it is difficult to recover due to its high water solubility [14]. Therefore, in this paper,  $\beta$ -CDP was cross-linked with the CTS molecular chain to obtain a cyclodextrin-modified CTS derivative to obtain a CTS/ $\beta$ -CDP complex with both desirable properties to reduce the content of  $Zn^{2+}$  in wastewater.

## 2 Materials and methods

### 2.1 Materials

$\beta$ -CD (Shanghai Huishi Biochemical Reagent Co, Ltd.); CTS (deacetylation degree 80.0%-95.0%) (Sinopharm Chemical Reagent Co, Ltd.); citric acid, sodium dihydrogen phosphate (Beijing Chemical Plant); PEG 400, glutaraldehyde, base sodium chloride (Tianjin Guangfu Fine Chemical Research Institute); distilled water, hydrochloric acid, sodium hydroxide, ethanol, CM, dicesol orange, zinc powder, ammonium acetate (all analytically pure).

### 2.2 Methods

#### 2.2.1 Preparation of $\beta$ -CDP

CM (2 g), 1 g PEG-400, 0.25 g  $NaH_2PO_4$ , and 10 g  $\beta$ -CD were placed into 250ml a beaker. Distilled water was added and heated until all compounds were fully dissolved, and then the solution was placed in a

constant-temperature air drying oven and removed after reaction completion. The resulting product was carefully ground in a porcelain emulsion, and then fully washed, suction filtration and dried with distilled water and anhydrous ethanol. The final dry product was carefully ground to obtain  $\beta$ -CDP [15-16]. The reaction time and temperature of the  $\beta$ -CDP were varied for single-factor tests to prepare  $\beta$ -CDP using the preparation conditions shown in Table 1.

**Table 1.** Single-factor experimental design of  $\beta$ -CDP preparation

Factor	Level				
	1	2	3	4	5
Reaction time /h	3.5	4	4.5	5	5.5
Temperature / $^{\circ}$ C	130	135	140	145	150

### 2.2.2 Preparation of CTS/ $\beta$ -CDP complex

A solution of CTS in hydrochloric acid and  $\beta$ -CDP dissolved in distilled water were weighed, and the two solutions were poured into a beaker. While slowly mixing, 25% glutaraldehyde solution was added to the beaker, and the mixture was stirred at a constant temperature. After reaction completion, the Precipitate was filtered, washed with ethanol, distilled water, and vacuum filtered. The filtrate was dried at 45  $^{\circ}$ C to a constant weight to obtain the CTS/ $\beta$ -CDP complex as a brown powder [17].

The CTS/ $\beta$ -CDP complex was prepared using different reaction temperatures, CTS-to- $\beta$ -CDP mass ratios, reaction times, and amount of added glutaraldehyde. The preparation conditions are shown in Table 2.

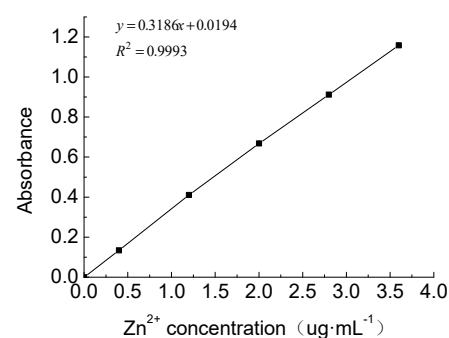
**Table 2.** Single-factor experimental design of CTS/ $\beta$ -CDP complex preparation

Factor	Level				
	1	2	3	4	5
Temperature / $^{\circ}$ C	60	70	80	90	100
Mass ratio	1:10	1:5	3:10	2:5	1:2
Reaction time /min	60	70	80	90	100
Glutaraldehyde addition /mL	1.0	1.5	2.0	2.5	3.0

### 2.2.3 Adsorption test and determination of optimal preparation conditions for CTS/ $\beta$ -CDP complex

The  $Zn^{2+}$  content was determined by the reaction of zinc and xylenol orange to form a stable orange-red complex at a weakly acidic pH of 6. The maximum absorption wavelength was 568 nm, the zinc content ranged from 0-3.2  $\mu$ g/mL, and the absorbance showed a good linear relationship [18].

The  $Zn^{2+}$  standard curve was obtained by placing 1.0, 3.0, 5.0, 7.0, and 9.0 mL of a 10  $\mu$ g/mL  $Zn^{2+}$  standard solution into a 25 mL volumetric flask. Then, 1.5 mL dimethylphenol orange and 3 mL acetic acid-ammonium acetate solution were successively added to adjust the absorbance, and then the  $Zn^{2+}$  standard curve was drawn.



**Fig. 1.**  $Zn^{2+}$  concentration standard curve

The CTS/ $\beta$ -CDP complex (0.2 g) obtained using different preparation conditions was added to 20 mL of 10  $\mu$ g/mL  $Zn^{2+}$  standard solution, shaken at 100 r/min at a constant temperature for 2 h, centrifuged, and then the supernatant was removed. The  $Zn^{2+}$  adsorption rate and adsorption amount were calculated by Equations 1 and 2:

$$\eta = \frac{C_0 - C_t}{C_0} \times 100\% \quad (1)$$

$$R = \frac{(C_0 - C_t) \times V}{m} \times 100\% \quad (2)$$

Where  $C_0$  is the initial  $Zn^{2+}$  concentration,  $C_t$  is the concentration after constant-temperature oscillation for 2 h,  $V$  is the volume of the  $Zn^{2+}$  solution, and  $m$  is the mass of the adsorbent. The  $Zn^{2+}$  adsorption capacity and adsorption rate of CTS/ $\beta$ -CDP complexes were compared under different preparation conditions to determine the optimal preparation conditions of CTS/ $\beta$ -CDP complexes.

### 2.2.4 Comparative study on the $Zn^{2+}$ adsorption capacity of CTS, $\beta$ -CD, $\beta$ -CDP, and CTS/ $\beta$ -CDP Complex

CTS,  $\beta$ -CD, and  $\beta$ -CDP (0.2 g) were weighed and added to 20 mL of 10  $\mu$ g/mL  $Zn^{2+}$  standard solution, shaken at 100 r/min for 2 h, centrifuged, and taken. The adsorption rate of the supernatant was determined and compared with the adsorption rate of the CTS/ $\beta$ -CDP complex under its optimal adsorption conditions.

### 2.2.5 Fourier-transform infrared spectroscopy (FTIR) characterization

CTS,  $\beta$ -CD,  $\beta$ -CDP, and CTS/ $\beta$ -CDP complexes under their optimal adsorption conditions, and CTS/ $\beta$ -CDP complex after  $Zn^{2+}$  adsorption were pressed into tablets with potassium bromide and analyzed using FTIR. The scanning range was  $4000 - 500 \text{ cm}^{-1}$ . The infrared spectra of each substance were analyzed to determine the changes to surface groups before and after synthesis and adsorption.

### 2.2.6 Scanning electron microscopy (SEM) characterization

CTS,  $\beta$ -CD,  $\beta$ -CDP, and CTS/ $\beta$ -CDP complexes and CTS/ $\beta$ -CDP complex after  $Zn^{2+}$  adsorption under optimal adsorption conditions were sprayed with gold on a copper sample holder to observe the morphology of the samples.

## 3 Results and analysis

### 3.1 Effect of reaction conditions on the amount of $\beta$ -CDP produced during the preparation of $\beta$ -CDP

#### 3.1.1 Effect of reaction time on the amount of $\beta$ -CDP produced

Fig. 2 shows that when the reaction time was 4.5 h, the amount of  $\beta$ -CDP produced reached 6.06 g, and then decreased with longer reaction times. At longer reaction times,  $\beta$ -CDP partially decomposed, and therefore the optimum reaction time was set to 4.5 h.

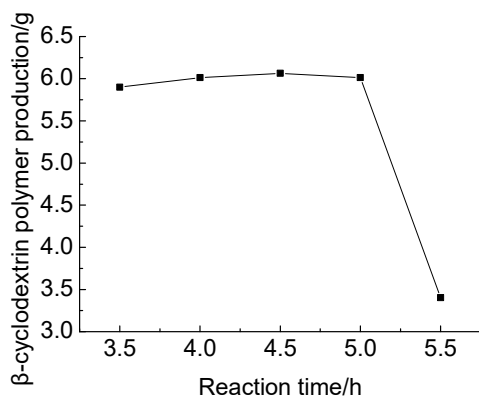


Fig. 2. Effect of reaction time on the amount of  $\beta$ -CDP produced

#### 3.1.2 Effect of reaction temperature on the amount of $\beta$ -CDP produced

Fig. 3 shows that when the reaction temperature was  $145 \text{ }^\circ\text{C}$ , the amount of  $\beta$ -CDP reached 6.58 g, and then decreased when the reaction temperature was increased further. This occurred because at higher temperatures, the reaction rate was lower, which decreased the amount of

product. Therefore,  $145 \text{ }^\circ\text{C}$  was used as the optimum reaction temperature to prepare  $\beta$ -CDP.

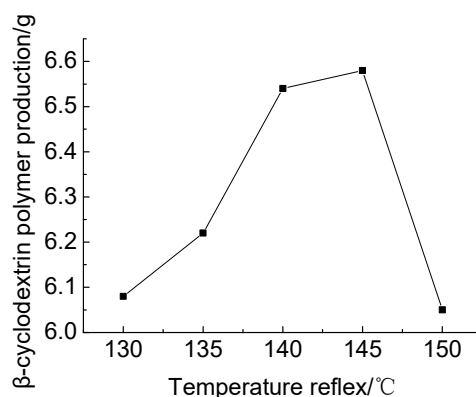


Fig. 3. Effect of reaction temperature on the amount of  $\beta$ -CDP produced

### 3.2 Effect of reaction conditions on the adsorption amount and adsorption rate of $Zn^{2+}$ during the preparation of CTS/ $\beta$ -CDP complex

#### 3.2.1 Effect of reaction temperature on $Zn^{2+}$ adsorption and adsorption rate

Fig. 4 shows that the adsorption amount and adsorption rate of  $Zn^{2+}$  increased with the reaction temperature. At a reaction temperature of  $80 \text{ }^\circ\text{C}$ , the adsorption amount and adsorption rate reached their highest values of  $34.93 \text{ mg}\cdot\text{g}^{-1}$  and 28.40%, respectively. Then, when the temperature was increased further, the adsorption amount and adsorption rate gradually decreased. This occurred because the temperature was too high, and part of the complex decomposed, and the synergistic effect of CTS and  $\beta$ -cyclodextrin complex was reduced, decreasing the adsorption amount and adsorption rate. Thus, the optimum reaction temperature was  $80 \text{ }^\circ\text{C}$ .

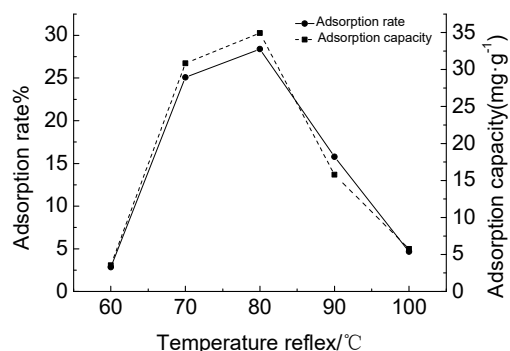


Fig. 4. Effect of reaction temperature on  $Zn^{2+}$  adsorption amount and adsorption rate

#### 3.2.2 Effect of mass ratio of CTS-to- $\beta$ -CDP on $Zn^{2+}$ adsorption amount and adsorption rate

Fig. 5 shows that the adsorption amount and adsorption rate of  $Zn^{2+}$  continuously increased with the mass ratio

of CTS-to- $\beta$ -CDP. When the mass ratio reached 3:10, the adsorption amount and adsorption rate of  $Zn^{2+}$  reached their highest values of  $97.70 \text{ mg}\cdot\text{g}^{-1}$  and 78.92%, respectively. However, they both decreased when the mass ratio of CTS-to- $\beta$ -CDP was increased further because the number of hydroxyl groups on the composite structure increased. This caused the composite surface to become negatively charged, and the adsorption amount and adsorption rate of  $Zn^{2+}$  continuously increased. However, when a certain mass ratio was reached, the excess  $\beta$ -CDP cross-linked with itself or dissolved, so that the number of hydroxyl functional groups on the structure of the composite was continuously reduced. This decreased the adsorption rate and adsorption amount. Therefore, the optimal mass ratio of CTS-to- $\beta$ -CDP was determined to be 3:10.

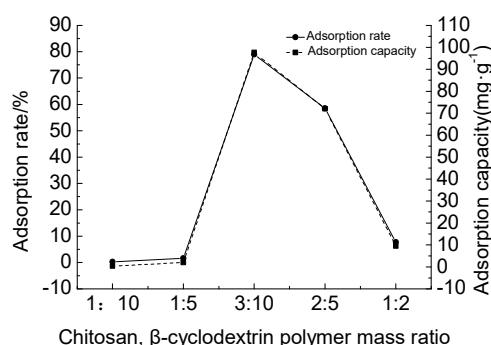


Fig. 5. Effect of mass ratio of CTS-to- $\beta$ -CD on the adsorption amount and adsorption rate of  $Zn^{2+}$

### 3.2.3 Effect of reaction time on $Zn^{2+}$ adsorption amount and adsorption rate

It can be seen from Fig. 6 that the adsorption amount and the adsorption rate reached their highest values of  $97.70 \text{ mg}\cdot\text{g}^{-1}$  and 78.92%, respectively at a reaction time of 90 min. At longer reaction times, the adsorption amount and the adsorption rate decreased due to shell aggregation at 90 min. The sugar completely reacted with the  $\beta$ -CDP, indicating that the optimum reaction time was 90 min.

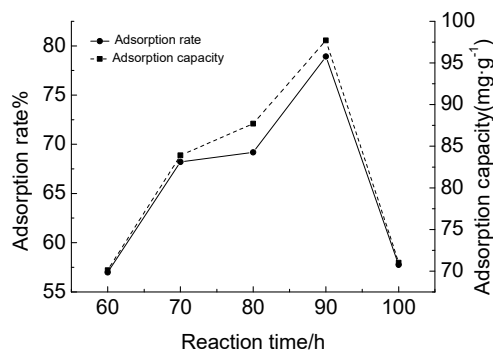


Fig. 6. Effect of reaction time on  $Zn^{2+}$  adsorption amount and adsorption rate

### 3.2.4 Effect of the glutaraldehyde amount on the adsorption amount and adsorption rate of $Zn^{2+}$

Fig. 7 shows that the adsorption amount and the adsorption rate gradually increased as more glutaraldehyde was added, reaching a maximum of  $97.70 \text{ mg}\cdot\text{g}^{-1}$  and 78.92% at 2 mL. Then, the adsorption capacity and adsorption rate of  $Zn^{2+}$  decreased with further increases in the amount of glutaraldehyde. This is because excess glutaraldehyde occupied more CTS active sites and  $\beta$ -CDP, resulting in insufficient amounts of CTS and  $\beta$ -CDP to chelate with  $Zn^{2+}$ . The optimum amount of glutaraldehyde in the reaction was therefore determined to be 2 mL.

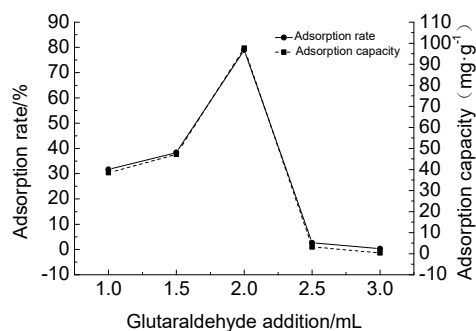


Fig.7. Effect of the amount of glutaraldehyde on the adsorption amount and adsorption rate of  $Zn^{2+}$

### 3.3 Comparison of $Zn^{2+}$ adsorption rates by $\beta$ -CD, $\beta$ -CDP, CTS, and CTS/ $\beta$ -CDP complex under optimal adsorption conditions

Fig. 8 shows that under the same adsorption conditions, the adsorption rate and amount of CTS/ $\beta$ -CDP complex on  $Zn^{2+}$  in solution were much higher than those of the other three substances. Thus, it can be concluded that CTS and  $\beta$ -CD have synergistic effects during  $Zn^{2+}$  adsorption from waste water.

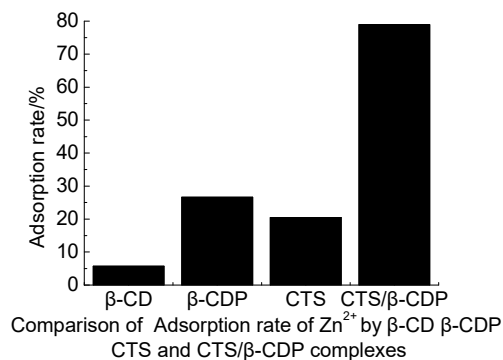


Fig. 8. Comparison of  $Zn^{2+}$  adsorption rates by  $\beta$ -CD,  $\beta$ -CDP, CTS, and CTS/ $\beta$ -CDP complex under optimal adsorption conditions

### 3.4 FTIR analysis of $\beta$ -CD and $\beta$ -CDP

The FTIR spectra in Fig. 9 show that the characteristic absorption peaks of  $\beta$ -CD and  $\beta$ -CDP are roughly the same, with strong and broad peaks generated by the hydroxyl group stretching vibration near  $3400 \text{ cm}^{-1}$ , and the characteristic absorption peaks of the  $\alpha$ -(1,4) glycoside and  $\alpha$ -(1,4) bonds of glucosamine at  $937.65$

$\text{cm}^{-1}$  and  $860.63 \text{ cm}^{-1}$ , respectively. The infrared spectrum of  $\beta$ -CDP showed an ester peak absorption peak at  $1708.33 \text{ cm}^{-1}$ . Thus, it was speculated that the carboxyl group of citric acid and the beta hydroxyl group reacted with one another to generate the ester bond of  $\beta$ -CD, confirming the successful synthesis of  $\beta$ -CDP.

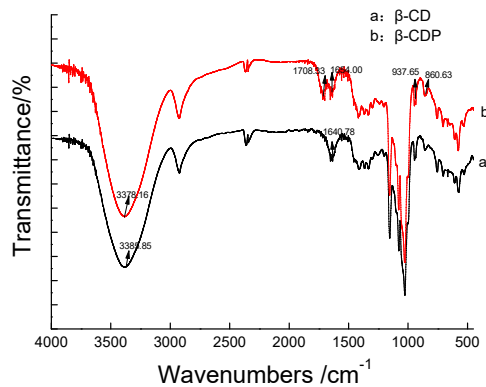


Fig. 9. FTIR spectra of  $\beta$ -CD and  $\beta$ -CDP

### 3.5 FTIR analysis of CTS, CTS/ $\beta$ -CDP complex and CTS/ $\beta$ -CDP complex after $\text{Zn}^{2+}$ adsorption

The FTIR spectra in Fig. 10 contain a peak at  $3426.79 \text{ cm}^{-1}$ , which was attributed to the stretching vibration of the hydroxyl groups of CTS, and  $895.72 \text{ cm}^{-1}$  is a characteristic peak of the  $\beta$ -(1,4) glycosidic bond of CTS. After the polymerization of  $\beta$ -CD, peaks appeared at  $937.65 \text{ cm}^{-1}$  and  $860.63 \text{ cm}^{-1}$ , which corresponded to the  $\alpha$ -(1,4) glycosidic linkages and  $\alpha$ -(1,4) glucopyranose absorption peaks of  $\beta$ -CDP, respectively. The infrared spectra of the polysaccharide and  $\beta$ -CDP contain a characteristic peak at  $895.43 \text{ cm}^{-1}$  which was the  $\beta$ -(1,4) glycosidic bond of CTS in the CTS/ $\beta$ -CDP complex. The peaks at  $947.57 \text{ cm}^{-1}$  and  $846.20 \text{ cm}^{-1}$  appeared due to the  $\alpha$ -(1,4) glycosidic linkages and the  $\alpha$ -(1,4) glucopyranose absorption characteristic peaks of  $\beta$ -CDP, respectively. Since CTS and  $\beta$ -CDP have many of the same functional groups, when they were crosslinked, CTS masked the  $\beta$ -CDP peaks, from which it can be inferred that  $\beta$ -CDP was successfully polymerized. The chitin was cross-linked with CTS to obtain a CTS/ $\beta$ -CDP complex.

By comparing the infrared spectra before and after  $\text{Zn}^{2+}$  adsorption, it can be seen that the absorption stretching peaks of the hydroxyl groups at  $3404.90 \text{ cm}^{-1}$  shifted to  $3424.42 \text{ cm}^{-1}$ , and the amine deformation and bending vibration peaks at  $1640.66 \text{ cm}^{-1}$  and  $1576.95 \text{ cm}^{-1}$ . After  $\text{Zn}^{2+}$  adsorption, these peaks increased and decreased to  $1640.76 \text{ cm}^{-1}$  and  $1553.87 \text{ cm}^{-1}$ , respectively. The hydroxyl bending vibration peak near  $1029.06 \text{ cm}^{-1}$  disappeared after adsorbing  $\text{Zn}^{2+}$ , and the absorption peaks at  $947.57 \text{ cm}^{-1}$  and  $846.20 \text{ cm}^{-1}$  also disappeared. It can be inferred that the  $\beta$ -CDP and  $\text{Zn}^{2+}$  of the complex also reacted, confirming that the active groups on the CTS/ $\beta$ -CDP complex were involved in

adsorption based on these peak changes. Thus, the complex was synthesized and reacted with  $\text{Zn}^{2+}$ .

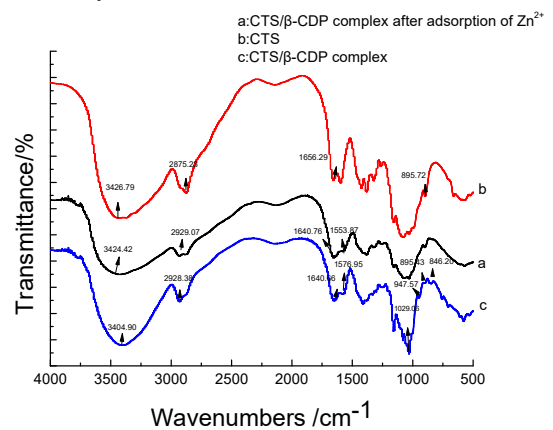
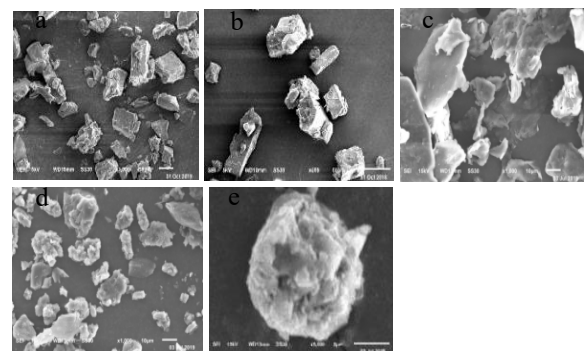


Fig.10. FTIR spectra of CTS, CTS/ $\beta$ -CDP complex, and CTS/ $\beta$ -CDP complex after  $\text{Zn}^{2+}$  adsorption

### 3.6 SEM analysis of $\beta$ -CD, $\beta$ -CDP, CTS, CTS/ $\beta$ -CDP complex, and CTS/ $\beta$ -CDP complex after $\text{Zn}^{2+}$ adsorption

As seen in Fig. 11, the surface of the  $\beta$ -CD was smooth and had a plate-like shape with many particles, while the modified  $\beta$ -CDP showed agglomeration and contained pores on its surface. The CTS had a flaky structure with a smooth surface and no wrinkles. The CTS/ $\beta$ -CDP complex had a solid particle structure, with a tight and rough surface, with a higher specific surface area than CTS, and an increased number of adsorption sites. After  $\text{Zn}^{2+}$  adsorption, the surface of the CTS/ $\beta$ -CDP complex became rougher, and it is speculated that many  $\text{Zn}^{2+}$  ions were adsorbed on its surface.



a:  $\beta$ -CD ( $50\mu\text{m}$ ); b:  $\beta$ -CDP ( $50\mu\text{m}$ ); c: CTS ( $10\mu\text{m}$ ); d: CTS/ $\beta$ -CDP complex ( $10\mu\text{m}$ ); e: CTS/ $\beta$ -CDP complex after  $\text{Zn}^{2+}$  adsorption ( $5\mu\text{m}$ )

Fig. 11. SEM analysis of  $\beta$ -CD,  $\beta$ -CDP, CTS, CTS/ $\beta$ -CDP complex, and CTS/ $\beta$ -CDP complex after  $\text{Zn}^{2+}$  adsorption

## 4 Conclusion

In this study, the optimum conditions for the adsorption of  $\text{Zn}^{2+}$  from waste water using a synthesized CTS/ $\beta$ -CDP complex were determined to be: a temperature of  $80 \text{ }^\circ\text{C}$ , a mass ratio of CTS-to- $\beta$ -CDP of 3:10, a reaction time of 90 min, and 2 mL glutaraldehyde.

The adsorption amount and adsorption rate of  $Zn^{2+}$  using the obtained complex reached a maximum of 97.70  $mg \cdot g^{-1}$  and 78.92%. In addition, the adsorption of  $Zn^{2+}$  in waste water using the CTS/ $\beta$ -CDP complex was much stronger than that of CTS,  $\beta$ -CD, or  $\beta$ -CDP under the same adsorption conditions.

The FTIR spectral analysis showed that an ester absorption peak at 1708.33  $cm^{-1}$  formed from the reaction of the carboxyl group of citric acid with the hydroxyl group on  $\beta$ -CD, indicating the successful synthesis of  $\beta$ -CDP. Peaks of the  $\beta$ -(1,4) glycosidic bond of CTS appeared in the infrared spectrum of CTS/ $\beta$ -CDP at 895.43  $cm^{-1}$  and 947.57  $cm^{-1}$ , while 846.20  $cm^{-1}$  was from the  $\beta$ -CDP  $\alpha$ -(1,4) glycosidic bond and  $\alpha$ -(1,4) glucopyranose absorption characteristic peak, indicating the successful synthesis of the CTS/ $\beta$ -CDP complex. The FTIR spectra before and after  $Zn^{2+}$  adsorption were different, and some characteristic peaks disappeared or shifted due to the adsorption of  $Zn^{2+}$ . SEM analysis showed that  $\beta$ -CDP was tighter than  $\beta$ -CD itself, and the surface of the CTS/ $\beta$ -CDP complex was rougher than CTS itself. The adsorption sites increased which increased the adsorption rate. Additionally, the CTS/ $\beta$ -CDP complex became rougher after adsorption due to the accumulation of many  $Zn^{2+}$  ions on its surface.

CTS and  $\beta$ -CD are natural products, and a CTS/ $\beta$ -CDP complex was prepared to adsorb  $Zn^{2+}$  by utilizing the metal ion adsorption capacity of CTS and the cavity structure of  $\beta$ -CD. When used to adsorb  $Zn^{2+}$  from waste water, the CTS/ $\beta$ -CDP complex was slightly more efficient than either CTS or  $\beta$ -CD individually. Additionally, this adsorption process is simple and low-cost, and cannot cause secondary pollution to the environment.

## Fund Project

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