Real-Time Determination of Overall Heat Transfer Coefficient from the Seebeck Effect by Using Adaptive Learning-Rate Optimization

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Abstract. It is challenging to determine the actual overall heat transfer coefficient under thermal conditions during processes. In a conventional approach, they are obtained as a constant with the empirical formula for the given conditions. In this study, the Adaptive moment estimation (Adam) technique is investigated for adaptive learning-rate optimization in the real-time determination of the overall heat transfer coefficient via the Seebeck effect in the thermoelectric modules. Two thermoelectric modules detect heat transfer as solid surfaces exposed to the outdoor air. The principle of energy balance and the Seebeck effect determine the overall heat transfer coefficients o ver time. The heating/cooling process of a co pper plate is considered with e xposure to the outdoor air. The overall heat transfer coefficient is determined with the proposed methodology over time. The temperature of the copper plate is numerically determined by the mathematical models with the obtained values of the overall heat transfer coefficient. It is confirmed that the calculated values of temperature are close to the measured values, with RMSE = 0.07 °C.

1 Introduction

In thermal analysis, the overall heat transfer coefficient is an important p arameter of h eat t ransfer in v arious engineering ap plications. S everal r esearch works have experimentally i nvestigated t he o verall h eat t ransfer coefficient, to improve the performance and efficiency of certain p rocesses. F or ex ample, an em pirical formula was used to increase the thermal efficiency and reduce energy consumption in thermal processes such as fintype h eat ex changes i n el ectronic d evices [1] an d t he heat loss of building facades [2], respectively. Recently, the d etermination of t he convective h eat t ransfer coefficient under actual convection processes over time has been proposed, using thermoelectric modules based on t he Seebeck e ffect [3]. I t was found that the convective heat t ransfer co efficient was d ependent o n time-variant properties of air and thermal surfaces. To determine t he convective h eat t ransfer co efficient, t he recursive o ptimization with t he gradient d escent technique is used to search for the actual values over time [4]. H owever, t he d ifficulty in e mploying t he gradient descent approach is that a reasonable step size is required to be adjusted in real time. To overcome this problem, th e A daptive moment e stimation (Adam) i s proposed t o d etermine t he o verall h eat t ransfer coefficient in t he o ptimization. P resently, t he A dam technique is one of the most effective adaptive learningrate optimization in deep learning models. T he A dam technique p rovided a f ast co nverge r ate with accu rate results [5]. A lso, a majority o f well-known de ep learning libraries supported the Adam technique, such as

Tensorflow, Keras, Caffe, Torch, etc. [6]. Therefore, the Adam te chnique i s a dapted w ith o ptimization for th e real-time d etermination o f the o verall heat t ransfer coefficient via the S eebeck effect in t his work. T his study i s a n e xperimental i nvestigation o f a heating/cooling p rocess with d ynamic e xposure t o t he outdoor air.

This paper is organized as follows. In Section 2, the Adam technique is presented for adaptive learning-rate optimization in the real-time determination of the overall heat transfer coefficients. In Section 3, the values of the overall h eat t ransfer co efficient i n t he heating/cooling process of a c opper plate in the o utdoor a ir a re determined o ver time by the proposed technique, as a case s tudy. T o v alidate t he ef fectiveness, t he Adam technique is applied to predict the temperatures of the copper plate du ring t he heating/cooling pr ocess i n outdoor a ir with mathematical models. A comparison between the measured t emperature and t he cal culated temperature, which are o btained with the o verall heat transfer coefficient, is shown. The conclusion about the viability of the proposed te chnique in the r eal-time determination of the overall heat transfer coefficient via the Seebeck effect is stated in Section 4.

2 Real-time determination of overall heat transfer coefficients by using adaptive learning-rate optimization

In thermal analysis, the overall heat transfer coefficient of a solid surface exposed to the outdoor air is comprised

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of a convective h eat t ransfer coefficient and a r adiant heat transfer coefficient [7], as expressed by:

$$h_T = h_c + h_r \tag{1}$$

where h_T is the overall heat transfer coefficient, h_c

is the convective heat transfer coefficient, and h_r is the radiant heat transfer coefficient.

To d etermine the o verall heat t ransfer co efficients over time, the Seebeck effect of a thermoelectric module is applied when the heat transfer takes place, as shown in Figure 1. O ne surface of the thermoelectric module is faced t o a n a ir a nd s unlight while a nother surface i s attached with a h eat s ink. T he p rinciple of en ergy balance i s u sed t o d etermine t he t emperature of t he ceramic substrate at the hot side:

$$m_{cs}c_{cs}\frac{dT_{ph,s}}{dt} = I - h_T A_T (T_{ph,s} - T_a) - Q_{T,s} \quad (2)$$

where m_{cs} is the mass of ceramic substrate, C_{cs} is the s pecific h eat o f cer amic s ubstrate, $T_{ph,s}$ is th e temperature o f cer amic substrate at the hot side, I is the i neident ir radiance o f sunlight, A_T is the s urface area o f t he t hermoelectric module, $Q_{T,s}$ is the he at transfer through t he t hermoelectric m odule w hen the cold side is induced by a heat sink, and t is the time.

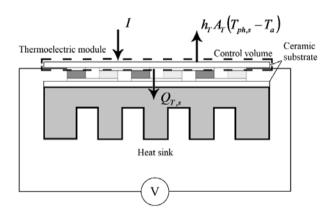


Fig. 1. Real-time determination of the overall heat transfer coefficients via Seebeck effect.

According to the S eebeck of fect [3], the S eebeck voltage of the thermoelectric module can be generated when there are temperature differences between the two ceramic s ubstrates of the thermoelectric module. T he amount of he at t ransfer t hrough t he t hermoelectric module is determined by:

$$Q_{T,s} = \frac{k_T}{\beta} V \tag{3}$$

where V is t he S eebeck voltage acr oss t he thermoelectric m odule, k_T is the thermal c onductivity coefficient of a t hermoelectric m odule, and β is the Seebeck effect coefficient.

The rate of h eat flowing through the thermoelectric module can be determined by the Seebeck voltage across the thermoelectric module. T he d irection of the h eat flow through the thermoelectric module is indicated by the p olarity of t he Seebeck voltage acr oss t he thermoelectric module.

According to equation (2), the values of the incident irradiance of s unlight and t he overall h eat t ransfer coefficient are unknown while the temperatures and the Seebeck voltage are measured. To determine the overall heat transfer coefficient, a nother thermoelectric module is attached in parallel, as shown in Figure 2. H owever, the heat sink is c hanged to a n i nsulated wall. T his modification r esults i n t he temperature d ifference between the two thermoelectric modules. With the same consideration, t he temperature of t he cer amic s ubstrate of the thermoelectric module coupled with an insulator at the hot side can be described as:

$$m_{cs}c_{cs}\frac{dT_{ph,i}}{dt} = I - h_T A_T (T_{ph,i} - T_a) - Q_{T,i}$$
(4)

where $T_{ph,i}$ is the t emperature of t he cer amic substrate at the hot side when an insulator is installed at the cold side, and $Q_{T,i}$ is the heat transfer through the thermoelectric module when the cold side is attached by an insulator.

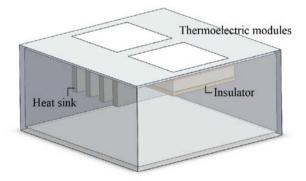


Fig. 2. Two thermoelectric modules coupled with heat sink and insulator.

Equation (2) is s ubtracted by e quation (4). The incident ir radiance of s unlight is e liminated. The temperatures of the ceramic substrates at the hot side are written as:

$$m_{cs}c_{cs}\frac{d(T_{ph,s}-T_{ph,i})}{dt} = -h_T A_T (T_{ph,s}-T_{ph,i}) - (Q_{T,s}-Q_{T,i})$$
(5)

The temperature d ifference b etween t he two thermoelectric modules at the h ot s ides i s d efined as $Y(t) := T_{ph,s}(t) - T_{ph,i}(t)$ with:

$$m_{cs}c_{cs}\frac{dY}{dt} = -h_T A_T Y - (Q_{T,s} - Q_{T,i})$$
(6)

The o verall h eat t ransfer co efficient can b e determined when the temperature difference between the two thermoelectric modules at the hot side in equation (6) is equal t o t he t emperature difference t hat i s o btained from the measurement. The error function is defined as:

$$E = \frac{1}{2} (Y(t) - Y_m(t))^2$$
(7)

where Y_m is the measured value of the temperature difference between the two thermoelectric modules. The backward finite difference a pproximation is a pplied t o equation (6).

$$\frac{Y(t) - Y(t - \Delta t)}{\Delta t} = -\frac{h_T(t)A_T}{m_{cs}c_{cs}}Y(t) - \frac{1}{m_{cs}c_{cs}}(Q_{T,s}(t) - Q_{T,i}(t))$$
(8)

where Δt is the time step.

According t o equation (9), t he cu rrent t emperature difference can be determined when the previous temperature difference is known.

$$Y(t) = \frac{Y(t - \Delta t) - \frac{\Delta t}{m_{cs}c_{cs}} (Q_{T,s}(t) - Q_{T,i}(t))}{1 + \frac{h_T(t)A_T \Delta t}{m_{cs}c_{cs}}}$$
(9)

By t aking t he d erivative of e quation (8), t he derivative of the temperature difference with respect to the overall heat transfer coefficient can be obtained as:

$$\frac{\partial Y(t)}{\partial h_T} = \frac{\frac{\partial Y(t - \Delta t)}{\partial h_T} - \frac{A_T \Delta t}{m_{cs} c_{cs}} Y(t)}{1 + \frac{h_T(t) A_T \Delta t}{m_{cs} c_{cs}}}$$
(10)

The derivative of the error function with r espect to the overall heat transfer coefficient can be determined by:

$$\frac{\partial E}{\partial h_T} = \frac{\partial E}{\partial Y} \frac{\partial Y}{\partial h_T} = \left(Y(t) - Y_m(t)\right) \left(\frac{\frac{\partial Y(t - \Delta t)}{\partial h_T} - \frac{A_T \Delta t}{m_{cs} c_{cs}}Y(t)}{1 + \frac{h_T(t)A_T \Delta t}{m_{cs} c_{cs}}}\right)$$
(11)

In this work, the adaptive moment estimation (Adam) algorithm is a pplied, to minimize the error function in equation (7):

$$h_T(t + \Delta t) = h_T(t) - \eta \frac{\hat{m}(t + \Delta t)}{\sqrt{\hat{\nu}(t + \Delta t)} + \varepsilon}$$
(12)

With the b ias c orrected e stimators for the first a nd second moments,

$$\hat{m}(t + \Delta t) = \frac{m(t + \Delta t)}{1 - \beta_1} \tag{13}$$

and

$$\hat{v}(t + \Delta t) = \frac{v(t + \Delta t)}{1 - \beta_2} \tag{14}$$

The moving a verages of gr adient and the moving averages of squared gradient are defined as:

$$m(t + \Delta t) = \beta_1 m(t) + (1 - \beta_1) \frac{\partial E}{\partial h_r}$$
(15)

and

$$v(t + \Delta t) = \beta_2 v(t) + (1 - \beta_2) \frac{\partial E}{\partial h_T}$$
(16)

where $h_T(t + \Delta t)$ is the u pdated v alue of the

overall heat transfer coefficient at the next time, $h_T(t)$ is the value of the overall heat transfer coefficient at the current time, η is the learning rate or step size, and ε is the empirical constant used to prevent division by zero in the i mplementation. β_1 and β_2 are t he h yper parameters of the algorithm, which are the exponential decay r ate for the first moment e stimates and t he exponential decay rate for the second-moment estimates, respectively.

The initial numerical values of the parameters are in Table 1. The derivative of the error function with respect t ot he overall h eat t ransfer co efficient i n equations (15) and (16) is determined by equation (11).

Table 1. Numerical values of parameters.

Parameters	Numerical values
Learning rate or step size, η	0.09
Empirical constants, \mathcal{E}	10 ⁻⁸
Running average of the gradient, β_1	0.9
Running average of the squared gradient, eta_2	0.999
Initial value of overall heat transfer coefficient, h_T	20
Initial value of moving average of gradient, m	0
Initial value of moving averages of squared gradient, V	0

3 Results and Discussion

To a pply t he pr oposed m ethodology i n r eal t ime, a n experiment for temperature p rediction of a co pper p late is set up, as shown in Figure 3.

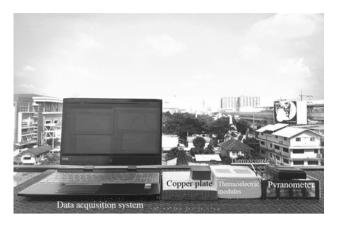


Fig. 3. Experiment of copper plate in outdoor air.

The copper plate is placed in an insulated box where a single surface is exposed to a tmosphere d uring the daytime. The temperature of the copper plate is governed by the energy balance equation, equation (17).

$$m_c c_c \frac{dT}{dt} = I - h_T A_c \left(T - T_a \right) \tag{17}$$

where T is the temperature of copper plate, m_c is the mass of copper plate, C_c is the specific heat of the copper plate, and A_c is the transferred area of the copper plate.

The p hysical p roperties o ft het hermoelectric modules and the copper plate are listed in Table 2. To solve equation (17), the overall heat transfer coefficient, incident irradiance, and air temperature must be known over time. The p roposed t hermoelectric modules ar e located n ear t he copper p late f or d etermining t he unknown overall heat transfer of the copper plate to air. A p yranometer (SolData98HP) with a n acc uracy o f \pm 3%FS, a nd a K -type t hermocouple ar e u sed f or measuring solar i rradiance o n a copper p late and ai r temperature, respectively

Table 2. Physical properties and parameters.

Parameters	Numerical values
Mass of ceramic substrate, m_{cs} (g)	4.0456
Specific heat of ceramic substrate, C_{cs} (J/g°C)	0.88
Seebeck effect coefficient, β (V/ °C)	0.0424
Thermal conductivity coefficient, k_T (W/ °C)	0.1639
Mass of copper plate, m_c (g)	28.672
Specific heat of copper plate, C_c (J/g°C)	0.385
Area of copper plate, A_c (m ²)	0.0016

The solar radiation flux density and air temperature are observed as illustrated in Figure 4(a). The proposed methodology i n S ection 2 i s i mplemented for determining t he va lues o f the o verall heat t ransfer coefficient over time. The values of the error function for computation performance are plotted against time in Figure 4 (b), as they are acceptably small. This result indicates that the calculated temperature differences are in good agreement with the measurements. As reported in F igure 4 (c), t he va lues o f t he o verall h eat tr ansfer coefficient ar e o btained o ver t ime. Together with t he incident i rradiance an d ai r t emperature, t he cal culated values of the overall heat transfer coefficient are inputted into the mathematical model of the c opper p late in equation (17). F igure 4(d) shows a comparison of the simulated r esults o f co pper p late t emperature with measured v alues. I t is o bserved t hat t he s imulated results o f co pper p late t emperature cl osely t rack t he measured values with RMSE = 0.07 °C. F urthermore, the simulated results with an estimated overall heat transfer co efficient of 20 W /m²K ar e comparatively presented with higher d eviations a s a c onventional approach.

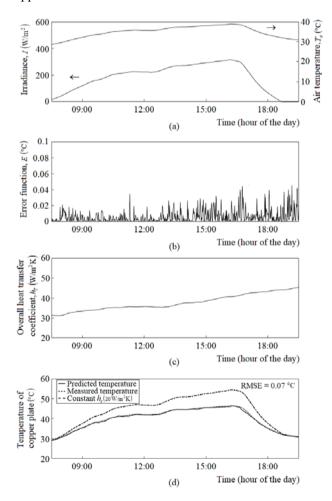


Fig. 4. Experimental results of temperature prediction for the copper plate over time: (a) irradiance and air temperature, (b) error function, (c) calculated overall heat transfer coefficient, (d) predicted and measured temperature of the copper plate.

4 Conclusion

The overall h eat t ransfer co efficient is a cr ucial parameter in determining the heat transferred between a surface and the outdoor air at different temperatures. In this study, t he Adam technique i s i nvestigated f or adaptive learning-rate optimization. This is used for the real-time d etermination o f the o verall heat t ransfer coefficients via the Seebeck effect in thermoelectric modules. Two thermoelectric modules detect heat transfer as solid surfaces are exposed to the outdoor air. The principle of energy balance and the Seebeck effect are used to determine the overall heat transfer coefficient over time. To demonstrate the viability of the proposed methodology in a real-time implementation, the values of the overall heat transfer coefficient of a copper plate in ambient conditions during the daytime are determined, to pr edict t he c opper plate t emperatures. T he temperatures are found to be in good agreement with the measured values, with RMSE = 0.07 °C. However, the predicted t emperatures from the es timated o verall h eat transfer co efficient o f 2 0 W/m²K do n ot fit measured temperatures.

References

1. A. B airi, Q uantification of t he na tural c onvective heat tr ansfer f or th e tilt ed a nd w ire-bonded QFN32b-PCB el ectronic as sembly, *Int. Commun. Heat Mass Transfer*, **72**, 84–89 (2016)

- 2. L.E. Mavromatidis, Study of c oupled t ransient radiation-natural co nvention h eat transfer acr oss rectangular cavities in the vicinity of low emissivity thin f ilms f or i nnovative b uilding E nvelope Applications, *Energy Build.*, **120**, 114–134 (2016)
- 3. N. Korprasertsak, and T. Leephakpreeda, Real-time determination of convective heat transfer coefficient via th ermoelectric modules, *Journal of Heat Transfer-Transactions of the ASME*, **139**, 8p (2017)
- 4. J. Naiborhu, a nd K . S himizu, D irect gr adient descent c ontrol f or g lobal s tabilization o f g eneral nonlinear c ontrol s ystems, *IEICE Transactions on Fundamentals of Electronics Communications and Computer Sciences*, **83**, 516-523 (2000)
- D.P. Kingma, a nd J.L. B a, Adam: A method f or stochastic optimization, *International Conference on Learning Representations*, 1–13 (2015)
- 6. M. A badi, et al., T ensorFlow: a system for largescale m achine l earning, *Proceedings of the 12th* USENIX Conference on Operating Systems Design and Implementation (OSDI'16), 265-283 (2016)
- 7. F.P. Incropera, an d D.P. D eWitt, *Fundamentals of Heat and Mass Transfer 6th ed.* (New Jersey: Wiley, 2007