Screening of Metal Modified HKUST-1 to Enhance Mercury Removal Efficiency

Mingjie Zhang^{1,2}, Hongzhe Li^{1,2}, Gang Yang^{2,3}, Jiahui Yu^{2,3}, Yipei Chen^{2,3*}

Abstract. In this work, HKUST-1 and different metal modified HKUST-1 materials were investigated in Hg⁰ removal performance under air condition. Results showed that the pristine HKUST-1 only has a mercury removal rate of around 20%. After metal modification of HKUST-1, the removal efficiency was significantly improved. Among different modification materials employed in this study, HKUST-1 modified by manganese chloride exhibited the highest Hg⁰ removal efficiency of 95% at 250 °C. This value is relatively high compared with most previously reported catalysts. In addition, this study reveals that the enhanced Hg⁰ removal efficiency results from the increase of Brønsted acid sites on the sample surface, which is vital to Hg⁰ removal. Furthermore, it is found that SO₂ produced little toxicity to Mn(Cl)/HKUST-1 in the presence of O₂. This is beneficial to remove Hg⁰ in the industrial flue gas, where SO₂ is a common component. Therefore, Mn(Cl)/HKUST-1 synthesized here is a promising catalyst for Hg⁰ removal.

1 Introduction

Mercury control has become increasingly important because mercury is a poisonous material that results in a detrimental impact on ecosystems and human beings [1]. Countries are beginning to develop documents to control mercury emissions. In 2015, China began to implement pollutant emission standards (GB13223-2011) [2], which put forward the mercury emission limit of 0.03 mg/m³. Mercury is mainly divided into three forms: particlebound mercury (Hg^p), gaseous divalent mercury (Hg²⁺) and elemental mercury (Hg⁰) [3]. Among these, Hg²⁺ can be removed by wet flue gas desulfurization device because of its high-water solubility. The electrostatic dust removal equipment can be used to remove Hg^p, while Hg⁰ exists in a stable form and persist for a long time due to its high volatility and low solubility [4]. Hg⁰ affects the growth of crops and contaminates aquatic life, it can also poison the brain and digestive tract when entering human body [5]. Therefore, there is a considerable interest in developing a novel catalyst to control the emission of elemental mercury (Hg⁰).

Many studies have indicated that a new material, metal organic framework material (MOF), has a good prospect of mercury removal due to its high porosity, large specific surface area and diverse structural morphology [6, 7]. HKUST-1 is a copper-based MOF material with each Cu²⁺ binds to a water molecule. The water molecules can be easily removed and thus generating open metal sites. Moreover, HKUST-1 shows a lot of acid sites on the surface which is beneficial to Hg⁰ adsorption and catalytic

oxidation [8, 9]. Chen et al. found that HKUST-1 exhibited superior Hg⁰ removal efficiency when adding HCl into the gas [9]. However, HCl was proved to be toxic and corrosive. Additionally, many researchers have reported that metal oxides like CeO_x and MnO_x et al. have excellent performance on Hg⁰ removal [10]. Therefore, it is speculated that modification by metal or metal oxides on HKUST-1 can improve the Hg⁰ removal performance. Furthermore, there is a certain amount of SO_x existed in the coal-fired flue gas and SO₂ is the major component. It is difficult for air pollution equipment (APCDs) to completely remove SO₂ Many reports demonstrated that SO₂ played a negative role in Hg⁰ removal. Hence, the effect of SO₂ on Hg⁰ removal is significant to study.

In this work, different metal modified HKUST-1 composites were prepared. MnCl2 was found to to be the optimal modification agent for HKUST-1 in terms of Hg⁰ removal performance. Moreover, the SO₂ effect on the Hg⁰ removal when using the optimal was also investigated.

2 Materials and Methods

All chemicals were purchased from Sinopharm and used directly without any treatment.

2.1 Preparation of samples

HKUST-1 powder preparation

The preparation of HKUST-1 was carried out by hydrothermal method as described in Ref [11]. Copper nitrate (Cu(NO₃)₂·3H₂O, 7.5 g) and trimetric (TMA, 4 g)

¹College of Environmental and Chemical Engineering, Shanghai University of Electric power, 200090 Shanghai, China

²New Materials Institute, The University of Nottingham Ningbo China, 315100 Ningbo, China

³Key Laboratory for Carbonaceous Wastes Processing and Process Intensification of Zhejiang Province, The University of Nottingham Ningbo China, Ningbo 315100, China.

^{*} Corresponding author: z2019011@nottingham.edu.cn.

were first dissolved in ethanol. The mixed solution was heated under stirring at 50 °C for 3 h. The mixture was then centrifuged to separate the solid. The solid was placed in an oven at 120 °C overnight. The dried powder was then washed by methanol to remove impurities. The final product was obtained after centrifugation and drying.

HKUST-1/Al₂O₃ preparation

A certain amount of $Cu(NO_3)_2 \cdot 3H_2O$ was dissolved in ethanol and impregnated on Al_2O_3 by incipient wetness impregnation method. It was heated at 50 °C for 3 h. Then, TMA was excessive impregnated on the product and the reaction was heated at 50 °C for another 3 h. Finally, the sample (HKUST-1/ Al_2O_3) was washed by methanol and dried at 120°C.

A/HKUST-1 preparation

A metal salt with a mass fraction of 10% was dissolved in ethanol and deionized water (40 mL, 1:1). About 1g of HKUST-1 was mixed into the solution. The mixture was stirred at room temperature and ambient pressure for 6 h. After drying at $100~^{\circ}\text{C}$ overnight, the solid was calcined at $250~^{\circ}\text{C}$ for 2 h under N_2 atmosphere. The samples referred in the following were denoted as HKUST-1 and A/HKUST-1, respectively. (A was europium nitrate, cerium nitrate, manganese nitrate, manganese acetate or manganese chloride).

2.2 Characterization of the samples

The structure of the solid phase was examined by powder X-ray diffraction (XRD SmartLab3KW) with a scanning rate of 0.02°/s. The scanning range is 5-40°. The temperature-programmed reduction with H₂/He test was conducted by a chemisorption analyser (H2-TPR Auto Chem | 2920). Around 0.05 g sample was used for each test. The test temperature was set from 50-500 °C at the heating rate of 10 °C /min in the flow of 2.5% H₂ in He. Thermal stability test was conducted by using the thermogravimetric analyser (TGA NETZSCH STA49 F3) under nitrogen atmosphere, and the temperature was heated from 30 °C to 600 °C at 10°C/min [12]. In-situ infrared diffuse reflectance Fourier transform spectroscopy (in-situ DRIFT VERTEX 70) was adopted to study the acid sites on the surface, with NH₃ as the probe molecule [13].

2.3 Hg⁰ catalytic oxidation performance evaluation

The Hg^0 removal performance evaluation device consists of a Tekran3300 Hg^0 continuous monitoring module, an elemental Hg^0 calibration module (3310), a dilution probe controller (3340), a sample controller (3320) and a fixed bed quartz (D=12 mm). Teflon pipelines and quartz reactors were selected to avoid mercury adsorbed to the equipment. The reaction temperature range is 30-300 °C with a heating rate of 2°C/min. The Hg^0 removal efficiency was calculated by the following equation:

$$E = \frac{[Hg^0]_{in} - [Hg^0]_{out}}{[Hg^0]_{in}} \times 100\%$$

3 Results and discussion

3.1 Activity comparison of HKUST-1 and HKUST-1/Al₂O₃

The Hg⁰ removal performance of HKUST-1 powder and HKUST-1/Al₂O₃ with the same amount of HKUST-1 were conducted. The concentration of Hg⁰ source was 30 µg/m³, and 1500ml/min flow rate of air was injected into the reactor. The comparison results were shown in Fig. 1. Before 112 °C, the Hg⁰ removal efficiency of powder HKUST-1 was lower than that of HKUST-1/Al₂O₃. This can be attributed to the distribution of HKUST-1 was more uniform than the powder. As the temperature continued to increase, the removal efficiency of powder HKUST-1 gradually increased, which reached the highest value of 31.15% at around 175 °C. Then the removal rate decreased gradually with the increasing temperature and kept stable between 250-300 °C. However, the removal efficiency of HKUST-1/Al₂O₃ dramatically declined after 112°C and became zero at 150°C. This is probably caused by the structure decomposition of HKUST-1 supported on Al₂O₃ under this reaction condition. This matches with its colour change observed from light blue to grey, which was not found for HKUST-1 powder.

During the Hg⁰ removal process for HKUST-1 powder, both adsorption and catalytic oxidation of Hg⁰ occurred. The oxidation reaction rate rose with the temperature increasing, while the adsorption rate decreased. According to the curve shown in Fig. 1, it can be inferred that the oxidation reaction dominates before 175°C. However, due to the limited adsorption capacity of HKUST-1, as well as the dropped adsorption rate at high temperature (>175°C), the whole Hg⁰ removal efficiency obviously went down.

By comparing the results for two materials, the conclusion can be drawn that HKUST-1 powder was superior to HKUST-1/Al₂O₃ for Hg⁰ removal performance. Therefore, powder HKUST-1 was selected as the pristine sample for the later modification.

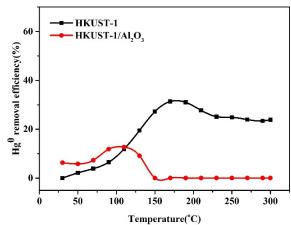


Figure 1 Dynamic activity test trend of prepared samples (Reaction condition: Hg⁰=30 μg/m³, GHSV=1.74×10⁵ h⁻¹, Temperature 30 -300 °C.)

3.2 Modified HKUST-1 for Hg⁰ removal test

Different metal salts were used to modify HKUST-1 and the Hg⁰ removal results were displayed in Fig. 2(a). It can be seen that Hg⁰ removal efficiencies of the samples modified are all higher than that of the sample without modification. When the temperature is higher than 200 °C, the high-to-low order of mercury removal rate is as follows: Mn/ HKUST-1 > Ce/HKUST-1 > Eu/HKUST-1 > HKUST-1. The material modified by manganese nitrate exhibited the highest mercury removal efficiency, reaching about 65%. This indicates that Mn is more helpful to improve the efficiency of Hg⁰ removal compared to the other metals. Many previous literatures have reported that Mn-based catalyst is one of the best candidate catalysts for the removal of Hg⁰[14]. Therefore, the Hg⁰ removal performance of manganese modified HKUST-1 was mainly studied.

The precursor is one of the important factors affecting the efficiency of adsorbent/catalyst. In this section, manganese nitrate, manganese acetate and manganese chloride were used to modify HKUST-1 (Mn(N)/HKUST-1, Mn(Ac)/HKUST-1 and Mn(Cl)/HKUST-1) respectively, and the results were displayed in Fig. 2 (b). The mercury removal efficiency of unmodified HKUST-1 increased with the increase of temperature, reaching its maximum value of 31.15% at 175 °C, and then remained basically flat between 20-30%. The mercury removal efficiency of the samples modified by different manganese precursors was higher than that of HKUST-1 during 30-300 °C. Among different kinds of manganese precursor, HKUST-1 modified by MnCl₂ shows the highest removal efficiency, up to 95% in the range of 250-300 °C, which could be attributed to the combined effect of Cu, Mn and Cl.

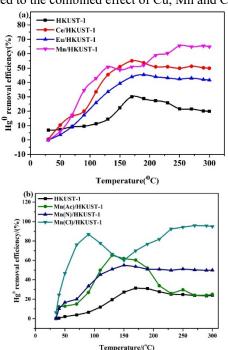


Figure 2 (a)Test of different metal modified HKUST-1 (b)Different manganese Mn precursors modification on HKUST-1 test results (Reaction condition: Hg⁰=30 μg/m³, GHSV=1.74×10⁵ h⁻¹, T= 30-300 °C)

3.3 Characterization of samples

3.3.1 XRD analysis

The XRD patterns reveal the crystallographic structures of the catalysts, as shown in Fig. 3. The pattern of HKUST-1 matches well with the simulated one, suggesting the material was prepared successfully with high purity [11]. There were still intact characteristic peaks of HKUST-1 after loading metals, indicating that the main structure was not affected by the impregnation loaded metal salt. In addition, there were no diffraction peaks of metal salts shown in the other three patterns. This means that Ce, Eu and Mn were well distributed and stayed as amorphous. The uniform dispersion of metal element was beneficial to Hg⁰ oxidation [15]. The low crystallinities of the modified materials were conducive to the formation of surface defects of the samples and thus providing more reaction sites [16]. Therefore, it was believed that metal modified HKUST-1 can remove Hg⁰ much more efficient compared to pristine HKUST-1 [17].

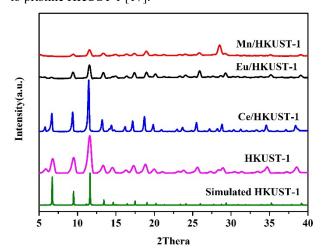


Figure 3 XRD pattern analysis

3.3.2 H₂-TPR experiment

It was reported that there was a close correlation between the reduction capacity and catalytic property of the catalyst [18]. Therefore, the H₂-TPR tests were conducted for four different metal-modified HKUST-1 samples to analyse their relative reducibility. As shown in Fig. 4, these four samples have peaks at different temperatures. Some distinctive peaks were displayed on the pattern. It can be found that two peaks appeared on the sample modified by Mn, at the temperature of 374 °C and 453 °C, which corresponded to the reduction process of Cu²⁺ to Cu⁺ and Mn⁴⁺ to Mn³⁺, respectively [19, 20]. Compared with pristine HKUST-1, the reduction temperature of Cu²⁺ was lower, indicating Mn/HKUST-1 has more oxygen species to improve catalytic oxidation performance. Correspondingly, Mn/HKUST-1 showed higher catalytic capacity than the other three samples due to the lower reduction temperature was favourable for higher catalytic performance [21]. Therefore, the H₂-TPR results gave explanation for the highest Hg⁰ removal efficiency of Mn/HKUST-1 among the four samples.

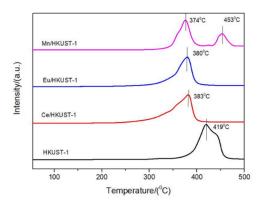


Figure 4 H₂-TPR test

3.3.3 Thermogravimetric analysis

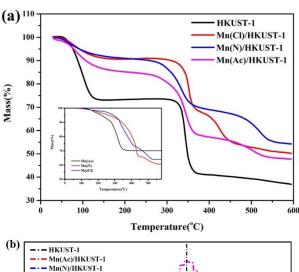
Thermal stabilities of prepared materials were identified by TGA (shown in Fig. 5(a)). Pristine HKUST-1 and modified HKUST-1 experienced similar processes. The first major mass loss before 120 °C was ascribed to the water molecules removal which were physically adsorbed. The second large mass decline after 300 °C was probably due to the decomposition of the HKUST-1 structure [22]. As a whole, HKUST-1 and modified HKUST-1 can keep the stable structure at a relatively high temperature.

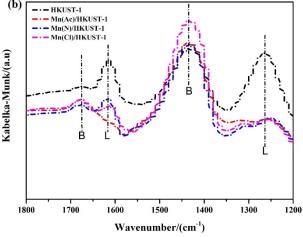
The additional weight loss stages of modified HKUST-1 compared to the pristine one was resulted from the decomposition of metal salts when temperature went higher than 350°C. This was in agreement with the TGA curves for different metal salts as shown in Fig. 5(a).

It can be found that HKUST-1 modified by MnCl₂ kept the last stable state at the highest temperature among three modified samples, indicating possessing the highest thermal stability, which is beneficial for Hg⁰ removal.

3.3.4 In situ DRIFTS

It was reported that Hg⁰ could combine with acid gas to form acid sites on the catalyst surface [23]. Therefore, in situ DRIFTS test was carried out to further study the active centres, the results were shown in Fig. 3(b). Some peaks displayed in the range of 1200-1700 cm⁻¹. Two peaks centred at 1260 cm⁻¹ and 1610 cm⁻¹ were attributed to the Lewis acid sites, and the bands at 1450 cm⁻¹ and 1670 cm⁻² ¹ were Brønsted acid sites [24]. The results showed that the largest amount of Brønsted acid sites presented on Mn(Cl)/HKUST-1 surface, which resulted in the excellent removal performance of Hg⁰. Fig. 3(c) shows the relative amount of Lewis acid sites and Brønsted acid sites corresponding to Fig.3(b). Papers have illustrated that Brønsted acid sites were prior to Lewis sites for Hg⁰ removal [25]. Hence, the in situ DRIFTS test also supported the result of the highest Hg⁰ removal performance of Mn(Cl)/HKUST-1.





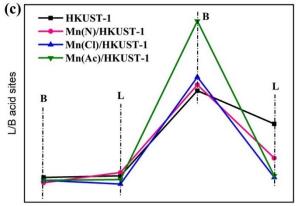


Figure 5 (a) Thermal stability test (b) In-situ DRIFT experiment (c) B/L acid sites ratio corresponding to (b)

3.4 The effect of SO₂ on Mn(CI)/HKUST-1

It is generally reported that SO₂ causes an inhibition of Hg⁰ removal [26]. Therefore, it is vital to study the SO₂ effect on the sample performance, since SO₂ normally exists in the flue gas. MnCl₂ modified HKUST-1, as the optimal Hg⁰ removal material obtained in this work were taken as the sample to investigate SO₂ effect on it. A typical temperature of 250 °C was selected to study SO₂ effect, since Hg⁰ removal efficiency reached the highest at this temperature. The efficiencies under three different gas conditions were investigated and the results are displayed in Fig. 6.

Under the first condition, the fresh catalyst was heated to 250 °C in N_2 for two hours. During this period, Hg^0 removal rate was found to be maintained at about 70%. Then it can be observed that the removal rate of Hg^0 gradually decreased after 100 ppm SO_2 was added into the gas at 120 min, dropping by 30% within two hours. It can be speculated that this phenomenon was caused by the competitive adsorption of SO_2 and Hg^0 on the surface of the sample. It was also reported that Hg^0 would compete adsorption with SO_2 in the literature [27].

For the second condition, 5% oxygen was added and it was found that the mercury removal efficiency could rise to about 95%. The above activity tests proved that a certain amount of O₂ could enhance the Hg⁰ removal efficiency. After stabilizing for two hours, 100 ppm SO₂ was also introduced. It was found that the removal efficiency of mercury still kept stable in the following two hours. This phenomenon indicated that O₂ could not only promote the removal of Hg⁰, but reduce the competitive adsorption of SO₂ [28]. It has been reported that part of SO₂ was converted to SO₃ in the presence of O₂, which promotes the catalytic oxidation of Hg⁰ to some extent, thus reducing the toxicity of SO₂ [29].

In order to further study Hg⁰ removal mechanism of Mn(Cl)/HKUST-1 with the presence of SO₂, the experiment under the third condition was carried out. The only difference between the second condition was that the fresh sample was pre-treated by 100 ppm SO₂ for 2 hours at room temperature before Hg0 removal test. As can be seen from the figure, the removal efficiency kept the same as the second condition during the first 120 min. However, the removal efficiency began to decrease afterwards. This phenomenon may due to the presence of some fresh Mnbased active sites on the surface of the pre-treated sample, which promotes the removal of Hg⁰. While Mn-based active sites were gradually poisoned with the continuous SO₂ injection. It is interested that the removal rate still reached around 60%, the reason was inferred to the new active sites generation on the surface to facilitate the removal of Hg⁰.

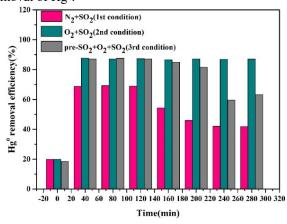


Figure 6 SO₂ effect on Mn(Cl)/HKUST-1 at 250°C

4 Conclusion

In conclusion, HKUST-1 and modified HKUST-1 were studied for Hg⁰ removal. Among these, Mn(Cl)/HKUST-1 showed the highest Hg⁰ removal efficiency of 95%, which

is competitive compared to most reported materials. The In-situ DRIFT result indicated that MnCl₂ promotes Brønsted acid sites generation, thus providing the beneficial factor for Hg⁰ removal. It is found that Mn distributed evenly on the HKUST-1 from the XRD result, which is favourable for Hg⁰ removal. Moreover, Mn(Cl)/HKUST-1 showed a good SO₂-resistance in the presence of O₂. Based on the screening results in this study, Mn(Cl)/HKUST-1 was proved to be a potential Hg⁰ removal material. Further studies on the mechanism of Hg⁰ removal by Mn(Cl)/HKUST-1 will be carried out in the future progress.

Acknowledgements

Following funding bodies are acknowledged for sponsoring this research: National Key R&D Program of China (2017YFB0603202), Ningbo 'Science and Technology Innovation 2025' Major Project (2018B10091) and Zhejiang Provincial Key Laboratory Programme (2020E10018).

Reference

- 1. Wang, S., et al., Atmospheric Chemistry and Physics, 2010. **10**(3): p. 1183-1192.
- 2. Emission standards for air pollutants from thermal power plants [S] GB13223. 2011.
- 3. Zhao, S., et al., Fuel, 2015. **158**: p. 891-897.
- 4. Presto, A.A. and E.J. Granite, Environmental science & technology, 2006. **40**(18): p. 5601-5609.
- 5. Fang, G.C., et al., Environ Monit Assess, 2011. **181**(1-4): p. 273-89.
- 6. Liu, Y., H. Li, and J. Liu, Fuel, 2016. 184.
- 7. Xiao, Z., et al., Journal of hazardous materials, 2016.
- 8. Chiericatti, C., et al., Mecroporous and mesoporous materials, 2012. **162**: p.60-63
- 9. Chen, D., et al., Fuel, 2018. 217: p. 297-305.
- 10. Kim, Y.J., et al., App Cat B :Environmental, 2012. 126
- 11. Chen, Y., et al., Progress in Natural Science: Materials International, 2018. **28**(5): p. 584-589.
- 12. Li, J., et al., Science Robotics, 2018. **3**(19).
- 13. Yang, G., et al., App Cata B: Environmental, 2019. 245
- 14. Zhang, A., et al., Chemical Engineering Journal, 2014. **236**: p. 29-38.
- 15. Li, H.H., et al., Chem.Pap, (2017) **71**:1569-1578
- Criado, M., A. Fernández-Jiménez, and A. Palomo, Microporous and Mesoporous Materials, 2007. 106(1-3): p. 180-191.
- 17. Li, H., et al., Chemical Papers, 2017. **71**(9): p. 1569-1578.
- 18. Torre-Abreu, C., et al., Applied Catalysis B: Environmental, 1997. **14**(3-4): p. 261-272.
- 19. Zhang, X., et al., Chemical Engineering Journal, 2017. **326**: p. 551-560.

- 20. Wan, Y., et al., Jour of Cata, 2004. 227(1): p. 242-252.
- 21. Zhang, X., et al., Molecular Catalysis, 2020. **482**: p. 110701.
- 22. Mu, X., et al., Microporous and Mesoporous Materials, 2018. **270**: p. 249-257.
- 23. Wilcox, J., et al., International Journal of Coal Geology, 2012. **90-91**: p. 4-20.
- 24. Lin, S.D., A.C. Gluhoi, and B.E. Nieuwenhuys, Catalysis Today, 2004. **90**(1-2): p. 3-14.
- 25. Zhao, H., et al., Environmental science & technology, 2016. **50**(2): p. 1056-1064.
- 26. Chen, Y., et al., Fuel, 2021. 285: p. 119064.
- 27. Li, H., et al., Fuel, 2020. 260: p. 116289.
- 28. Li, J., et al., Environ Sci & technology, 2010. **44**(1): p. 426-431.
- 29. Li, H., et al., Fuel, 2017. 208: p. 576-586.